

Design and Optimization of Structured Multi-Functional Trapping Catalysts for Conversion of Hydrocarbons and NOx from Diesel and Advanced Combustion Engines



Mike Harold (PI), Lars Grabow (University of Houston)

Bill Epling (CoI; University of Virginia)

Cary Henry, Robert Henderson, Minnie Lahoti (SwRI)

Todd Toops (Oak Ridge National Laboratory)

Sharan Sethuraman (Johnson Matthey Inc.)

Kiran Premchand (FCA Inc.)



ACE129

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Overview

TIMELINE

- Start: October 1, 2017
- End: September 30, 2020
- ~40% complete

BUDGET

- Total project funding
 - DOE: \$2,103,549
 - UH & partners: \$245,311
- Funding received
 - FY19: \$1,285,527

BARRIERS/TARGETS

- Develop robust emission control for advanced low temperature combustion (LTC) engines
- Achieve light-off for CO + HC oxidation below 150 °C while maintaining NOx emissions at 0.2 g/bhp-h
- “Cold start” increasingly important source of emissions: Cannot achieve 2025 regulations without new strategy for NOx & HCs
- Passive NOx adsorbers (PNAs): new concept requiring development and optimization
- Hydrocarbon traps (HCTs) not fully realized, especially in combination with PNA

PARTNERS

- U. Houston (lead)
- University of Virginia
- Johnson Matthey Inc.
- Southwest Research Institute
- Oak Ridge National Lab
- FCA Inc.

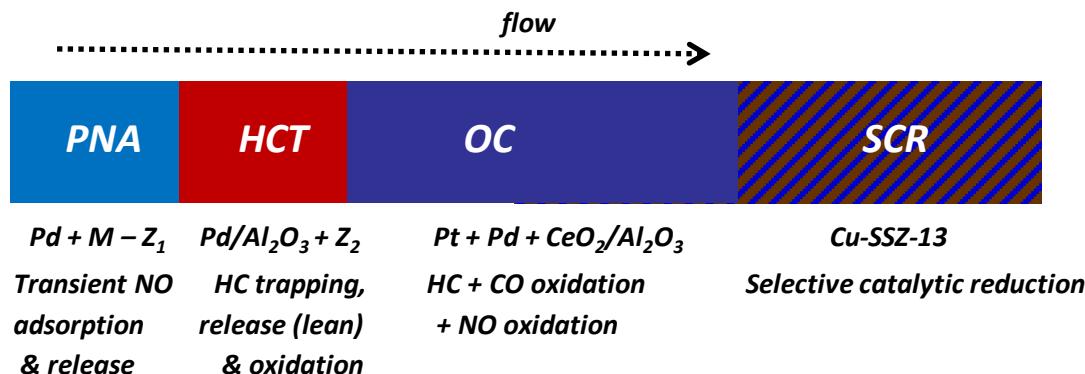


Project Objective

Research, develop, and demonstrate a multi-functional, catalyzed trap that will enable vehicles with advanced combustion strategies to meet Tier 3 emissions standards while achieving the 150 °C challenge for sustained co-oxidation of HC_s and CO and ≥90% NO trapping and release during warmup. Develop the

LHCNT = Lean HydroCarbon NOx Trap

to reduce emissions of HC_s and NOx from advanced combustion engines.



Approach and Collaborations

• University of Houston

- *Mike Harold (PI), Lars Grabow*
- Flow reactor catalyst evaluations; Computational catalysis (DFT); Kinetic & reactor modeling



• University of Virginia

- *Bill Epling (Col)*
- Hydrocarbon trap and catalyst deactivation



• Oak Ridge National Laboratory

- *Todd Toops, Jim Parks*
- New catalyst formulation and evaluations



• Johnson Matthey Inc.

- *Sharan Sethuraman*
- Baseline catalyst synthesis & characterization



• Southwest Research Institute

- *Cary Henry, Bob Henderson, Minnie Lahoti*
- Combustion and emission product speciation



• Fiat Chrysler Automobiles Inc. (FCA)

- *Kiran Premchand*
- Scale-up and vehicle testing of LHCNT prototype



1. Discovery, Synthesis,
Characterization and Screening
of Adsorbents and Catalysts

**Next
Generation
Emission**

**Device for Low
Temperature
Compression**

**Ignition
Engines**

2. Mechanistic and
Kinetic Modeling
Studies

3. Flow Reactor
Testing and
Parametric
Studies

4. Monolithic
Reactor Model
Development,
Validation &
Simulations

5. Feed Composition
Effects of Different Fuels

6. Identification of
Best Trapping and
Catalytic Materials
Benchmarked to
Model Materials

7. Prototype Device
Testing on LTC and
CDC Engine Exhaust

8. Materials and
Reactor Optimization

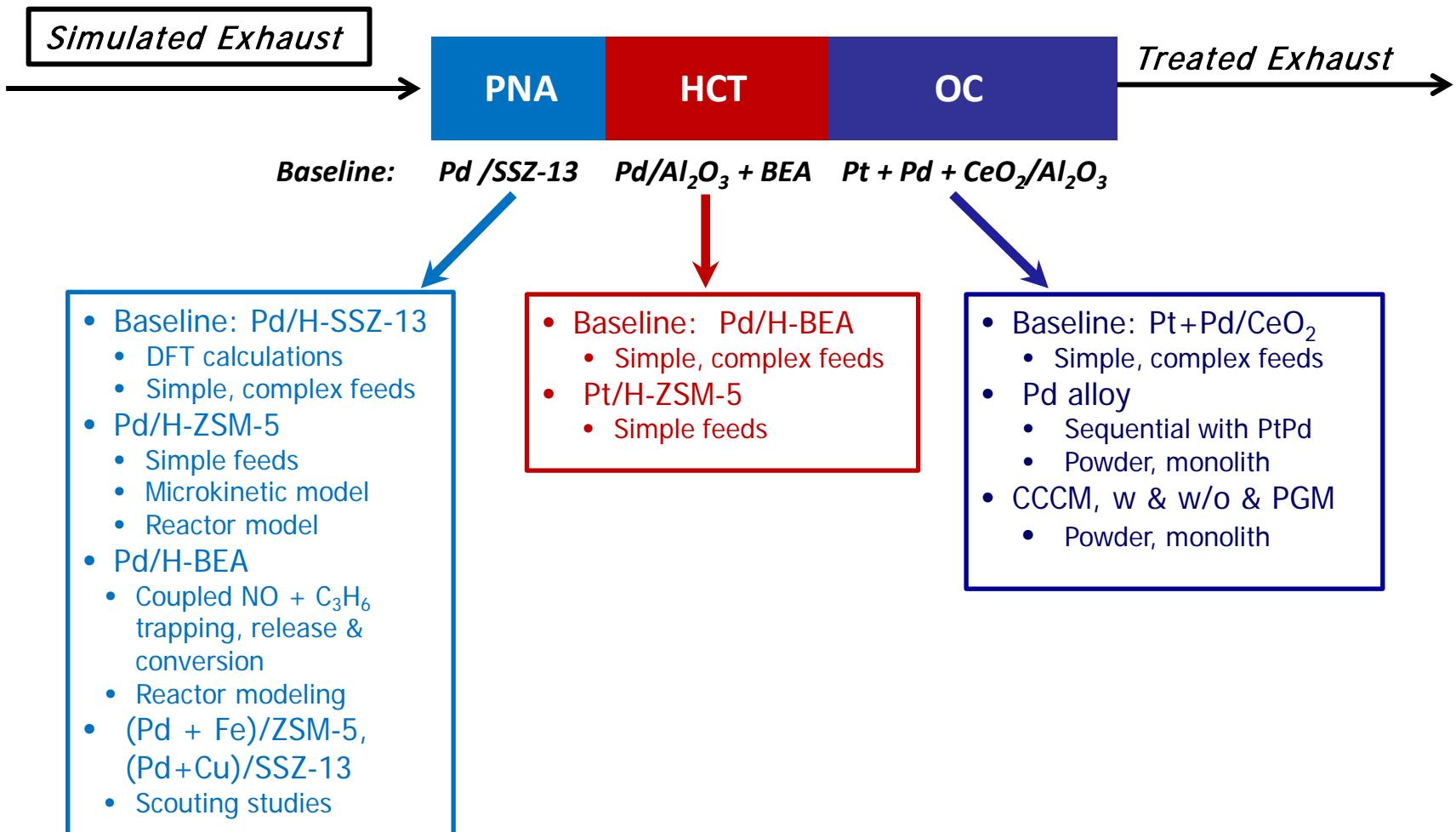


BP1 Milestones

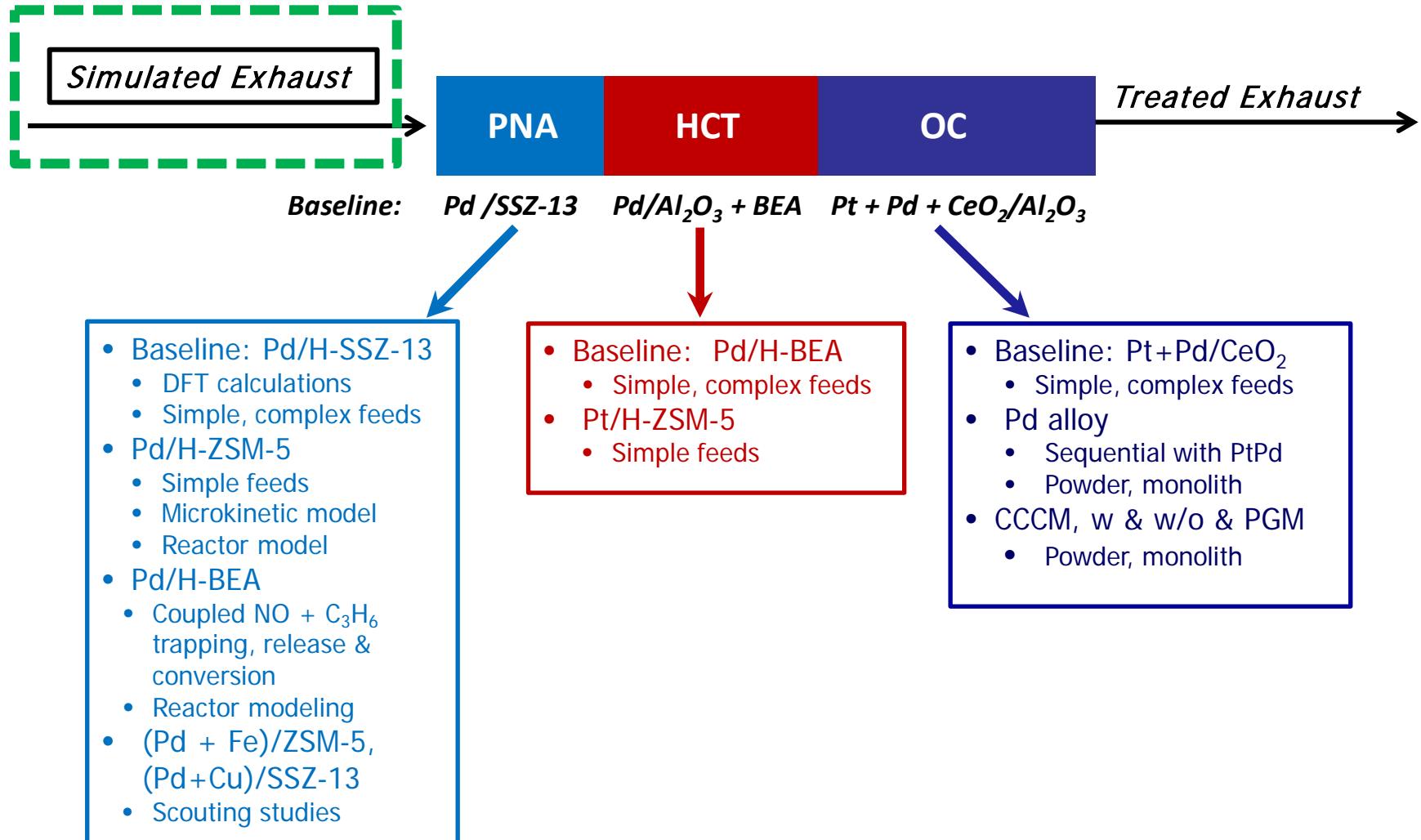
BP1-M#	Milestone	Type	Description	Status
BP1-M1	Material discovery	Technical	Identify at least one material each for HC trapping, HC oxidation, and NO adsorption from descriptor-based DFT.	Completed for HC oxidation, NO adsorption
BP1-M2	Baseline material performance testing complete	Technical	Complete flow reactor performance testing of the baseline LHCNT material in terms of quantifying sustained low temperature oxidation activity, NO trapping and release coupled with HC trapping and oxidation.	Completed for PNA; HCT and oxidation
BP1-M3	Exhaust speciation completed	Technical	Complete exhaust speciation for gasoline, diesel, and ethanol+gasoline blends.	Completed for diesel; to be completed in 4Q
BP1-M4	Kinetic model validated	Technical	Develop, tune and validate monolith reactor model containing the global kinetics of the baseline LHCNT material.	Kinetic/reactor model complete for NO trapping on Pd/ZSM-5; Pd/BEA, coupled NO + HC trapping
BP1-Go/NoGo	Identification of candidate material completed	Go/No Go	Identify at least one LHCNT material that, by 150°C, achieves light-off of the USDRIVE feed mixture and 90% NO trapping and release.	Baseline PNA (Pd/SSZ-13) + OC (Alloy/SiO ₂) meet NO trapping and low temp. light-off targets.



Project Activities

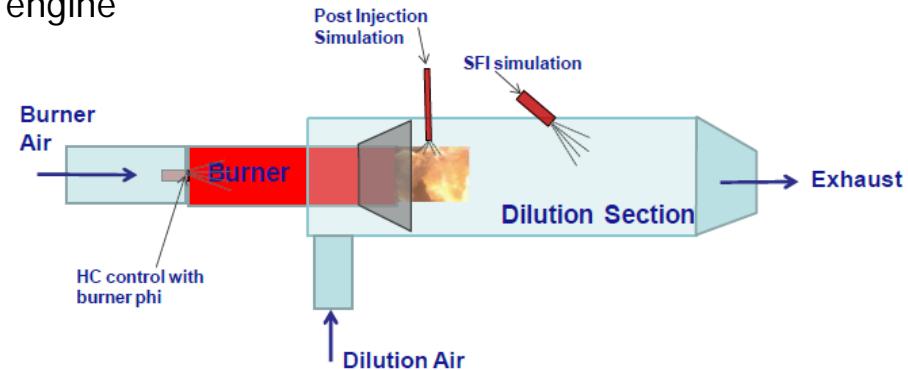


Project Activities

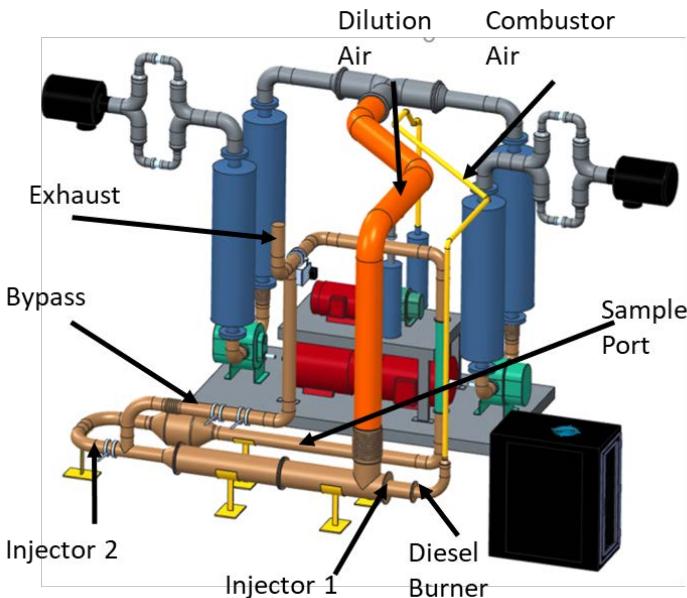


Exhaust speciation benchmarking

- Hydrocarbon speciation data for ~2013 era diesel engine
- Varied RPM (1375 – 2125), loads (25-50%)
- To be compared with
 - USDRIVE clean diesel protocol
 - Advanced low temperature diesel
 - Low temperature gasoline with EGR
- Equipment & methods
 - ECTO-Lab (SwRI) combustion test stand
 - Emission sample bags
 - Analytical: ~200 species measured using GC, GC-MS

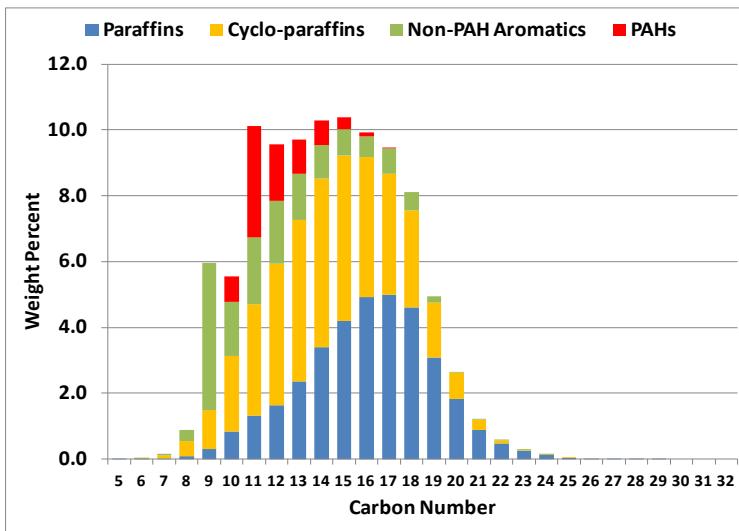


ECTO-Lab = Exhaust Composition Transient Laboratory



Exhaust speciation benchmarking

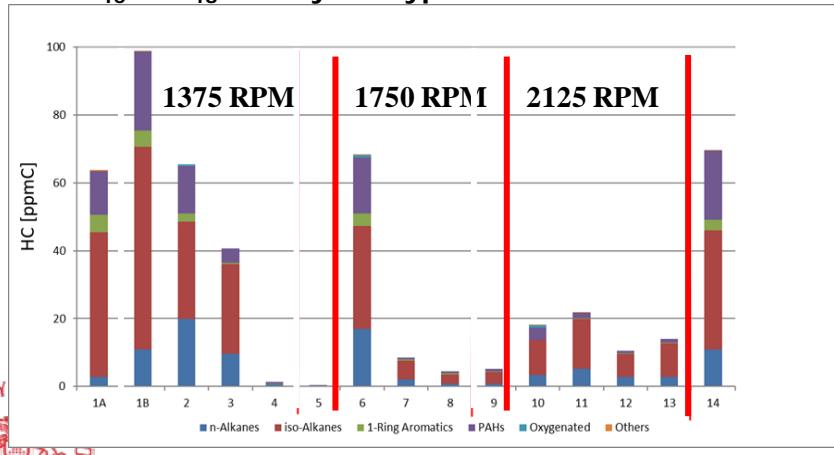
Diesel Speciation by Carbon Number and Molecule Type



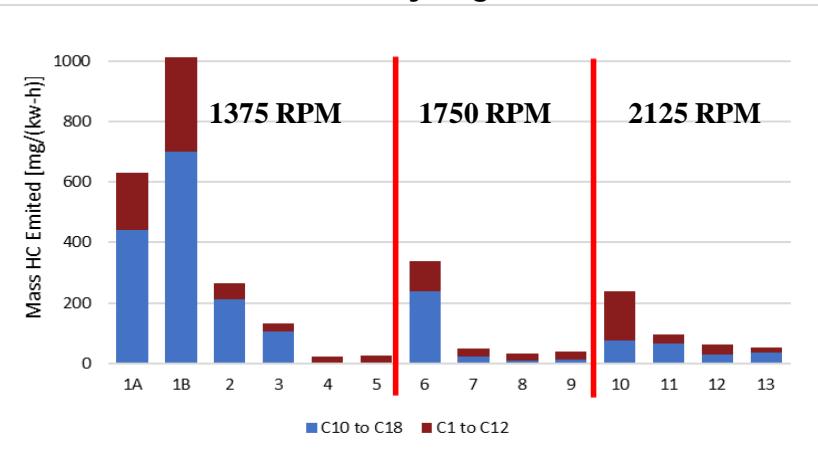
Engine Test Conditions

Speed [RPM]	Load Fraction [-]	Mode	Load [N-m]	Duration [s]
1375	10%	1A	120.74	1500.2
	10%	1B	120.34	1500.1
	25%	2	300.8	1500.2
	50%	3	601.96	1500.1
	75%	4	901.43	1500.2
	Full	5	1198.66	1500
1750	25%	6	293.25	1500.2
	50%	7	588.31	1500.1
	75%	8	879.99	1500
	Full	9	1168.13	1500
2125	25%	10	249.36	1500.1
	50%	11	497.67	1500.1
	75%	12	745.41	1500
	Full	13	994.72	1500
800	Idle	14	0.73	1500.1

C₁₀ to C₁₈ HCs by HC Type for Each Mode

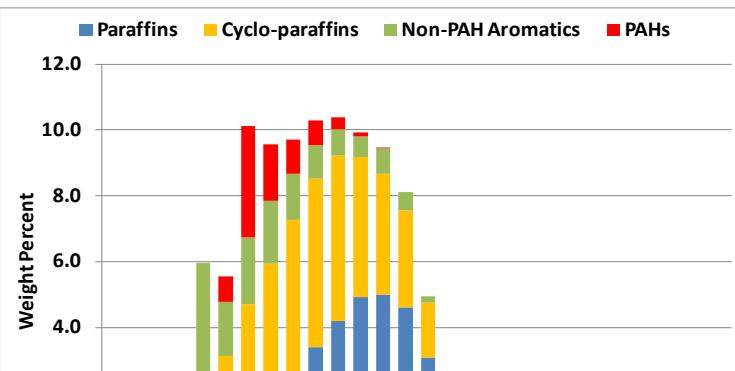


Mass of HCs Emitted Divided by Engine Power for Each Mode



Exhaust speciation benchmarking

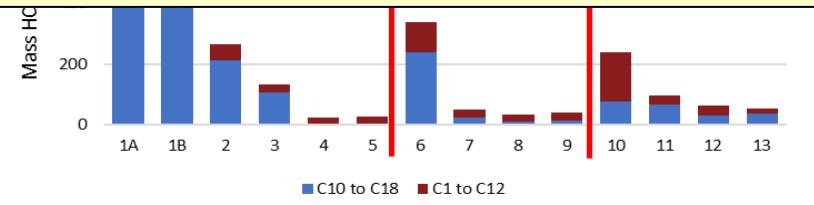
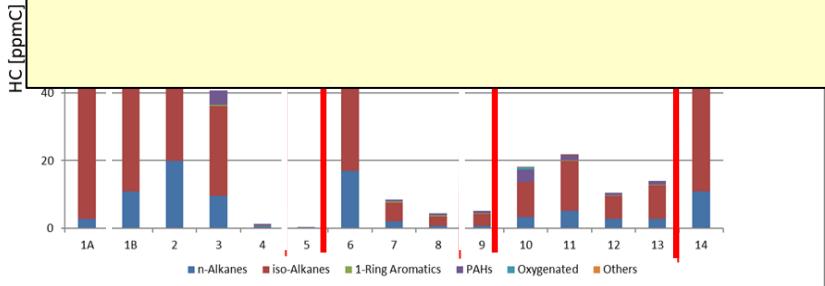
Diesel Speciation by Carbon Number and Molecule Type



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- Lights: C_2H_2 , C_2H_4 , C_3H_6 are main olefins
 H_2CO important component
 1,2-Dimethyl-3-Ethylbenzene most prominent aromatic
- Heavies: Iso-alkanes and polyaromatic hydrocarbons
 15 to 80% of total HCs; decreasing with speed & load



Materials and Conditions

Catalytic Materials

PNA: 1 wt.% **Pd** / **SSZ-13** (90%), Al₂O₃ (10%), 1.5 g wc/in³ (**Baseline**)
1 wt.% **Pd** + 1 wt.% **Cu** / **SSZ-13** (90%), Al₂O₃ (10%), 1.5 g wc/in³ (**New**)
1 wt.% **Pd** / **ZSM-5** (90%), Al₂O₃ (10%), 1.5 g wc/in³
1 wt.% **Pd** + 1 wt.% **Fe** / **ZSM-5** (90%), Al₂O₃ (10%), 1.5 g wc/in³ (**New**)
2 wt.% **Pd** / **BEA** (90%), Al₂O₃ (10%), 1.5 g wc/in³

HCT: 1 wt.% **Pd** / **BEA** (90%), Al₂O₃ (10%), 1.5 g wc/in³ (**Baseline**)

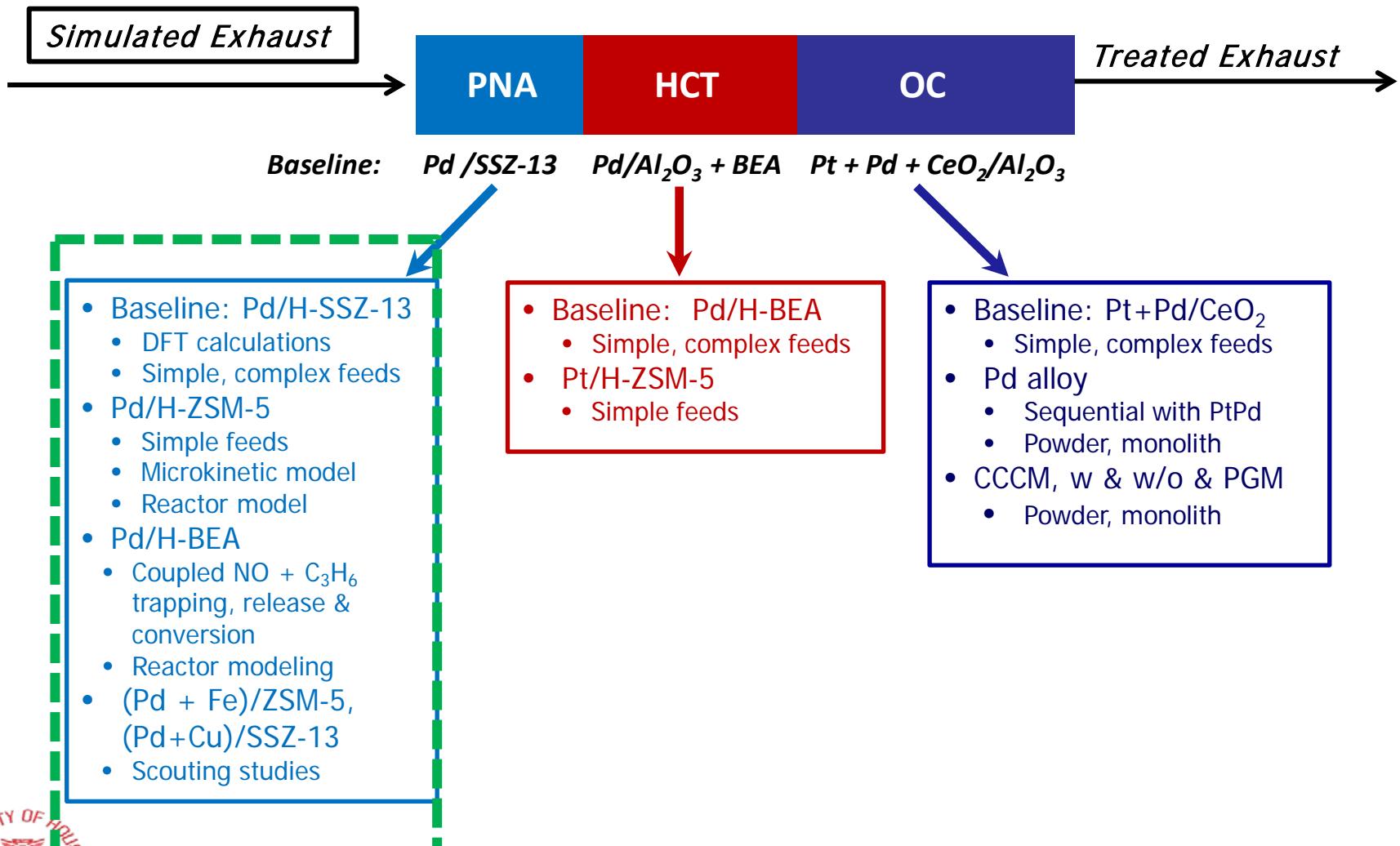
OC: **Pt**(0.5 wt.%)/**Pd**(0.5 wt.%) / **CeO₂**(15%), Al₂O₃ (85%), 1.5 g wc/in³ (**Baseline**)
'CCC' = **CuO** + **Co₂O₃** + **CeO₂** ternary oxide (varied compositions) (**NEW**)
Pd Alloy/SiO₂ (patent disclosure in preparation) (**NEW**)

Simulated Emission Feeds

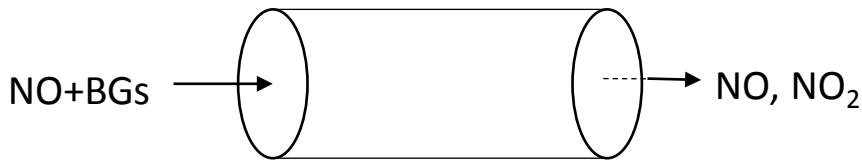
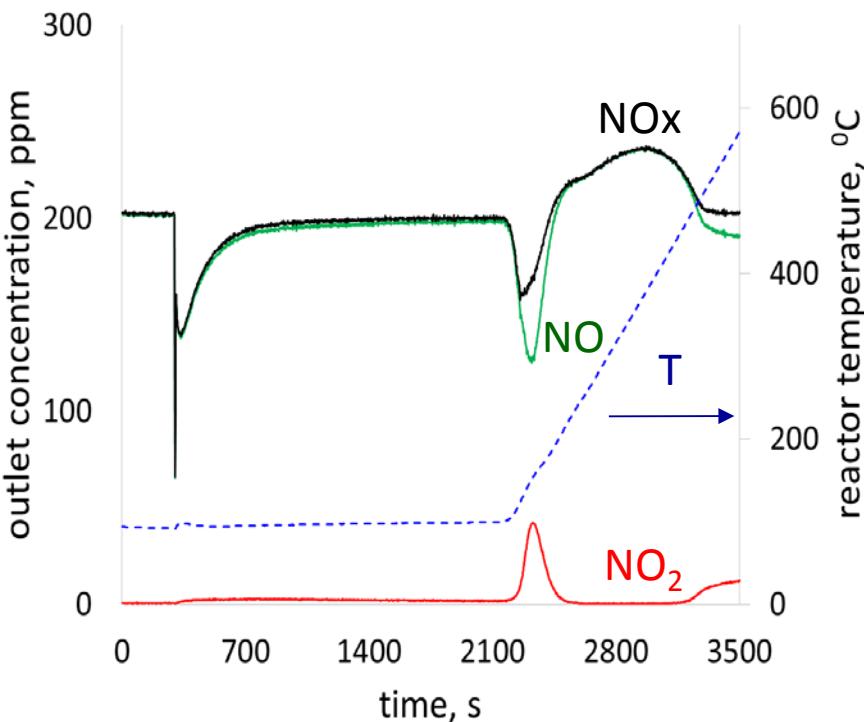
	O₂	H₂O	CO₂	NO	CO	H₂	C₂H₄	C₇H₁₂	C₁₂H₂₆				
Complex (USDRIVE)	12%	6%	6%	200 ppm	500 ppm	100 ppm	200 ppm	43 ppm	58 ppm				
Hybrid	12%	6%	6%	200 ppm	<i>Varied combinations & concentrations</i>								
Simple	12%	6%	6%	200 ppm	X	X	X	X	X				



Project Activities



NO uptake and release

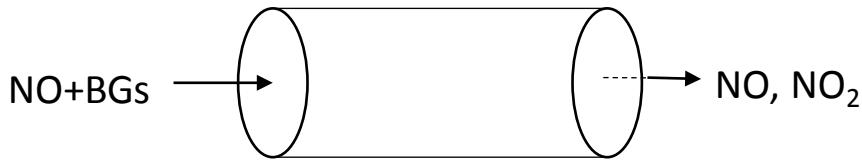
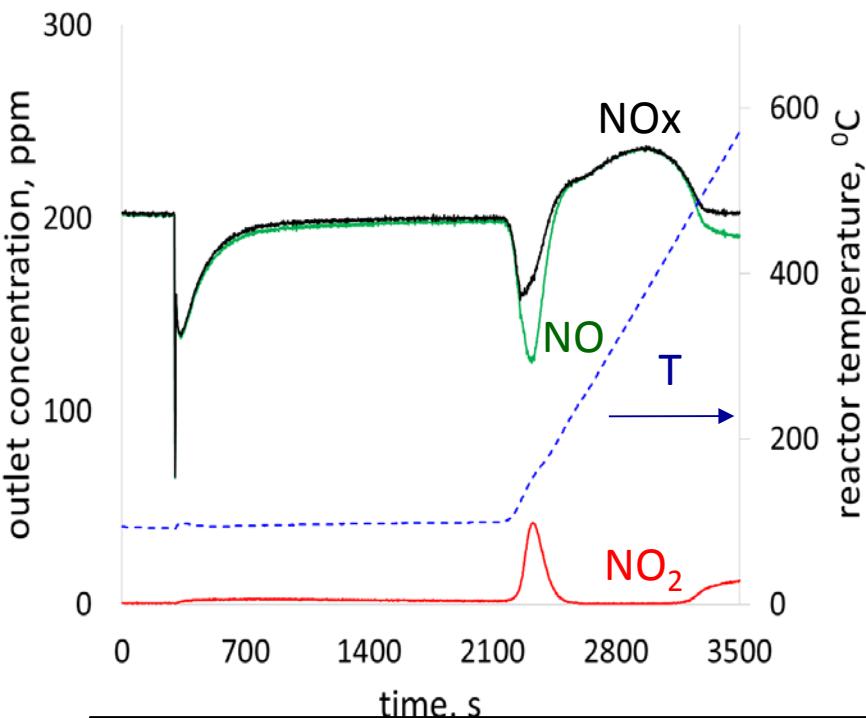


- H₂O competes for adsorption on Brønsted acid sites
- Two NO adsorption areas
 - *Low temp*: adsorption on Pd²⁺ and/or [Pd^{II}OH]⁺
 - *High temp*: adsorption on Pd²⁺, [Pd^{II}OH]⁺, Pd⁺, & Brønsted acid sites (freed by the water desorption)?
- NO₂ release immediately after the temperature ramp
- NOx released at temperatures higher than 200°C

NOx (ads)/NOx(des)	NOx/Pd
~ 1	~ 1



NO uptake and release



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- Two NO adsorption areas
 - *Low temp*: adsorption on Pd²⁺ and/or [Pd^{II}OH]⁺
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- Baseline PNA effective in trapping NO for simple & complex feeds

NOx (ads)/NOx(des)	NOx/Pd
~ 1	~ 1

NO₂ release immediately after the

temperature ramp

- NOx released at temperatures higher than 200°C



NOx trapping efficiency

Instantaneous trapping efficiency:

$$\eta = \left(1 - \frac{F_{NOx}}{F_{NO_{in}}} \right)$$

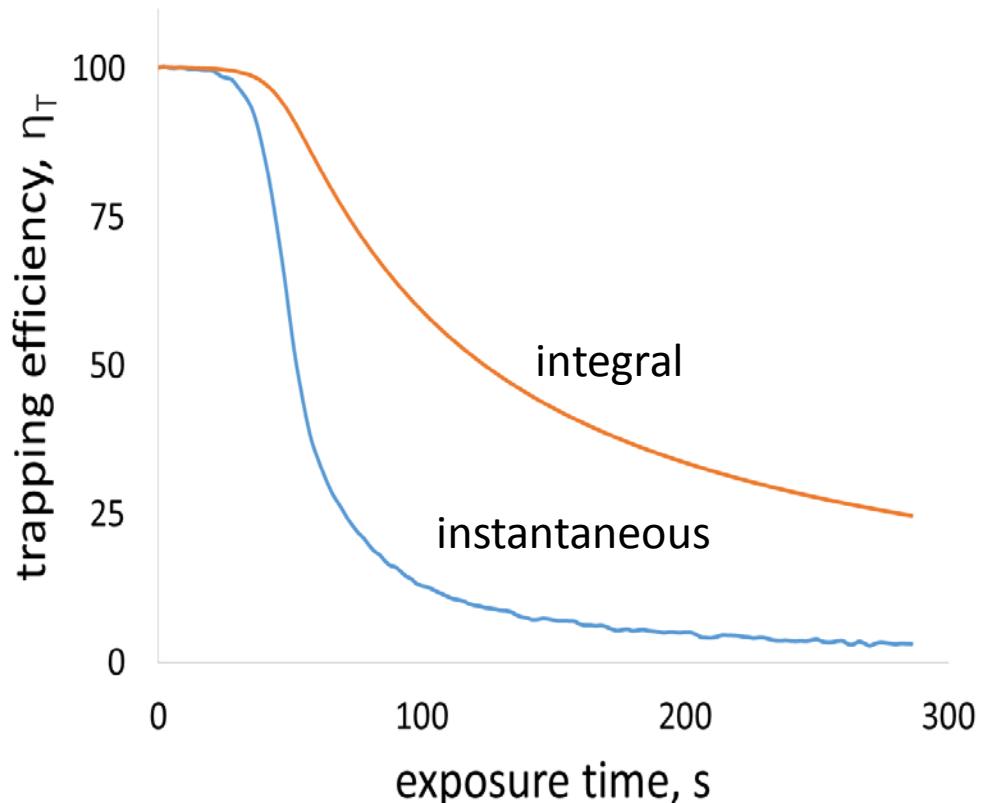
Integral trapping efficiency:

$$\eta_T = \frac{1}{\tau} \int_0^\tau \left(1 - \frac{F_{NOx}}{F_{NO_{in}}} \right) dt$$

Breakthrough time $\sim 60s$

NO/Pd ~ 1 in wet feed conditions

→ Efficient material for NOx trap and release



NOx trapping efficiency vs. exposure time
@ 100 C and GHSV = 30,000 hr⁻¹



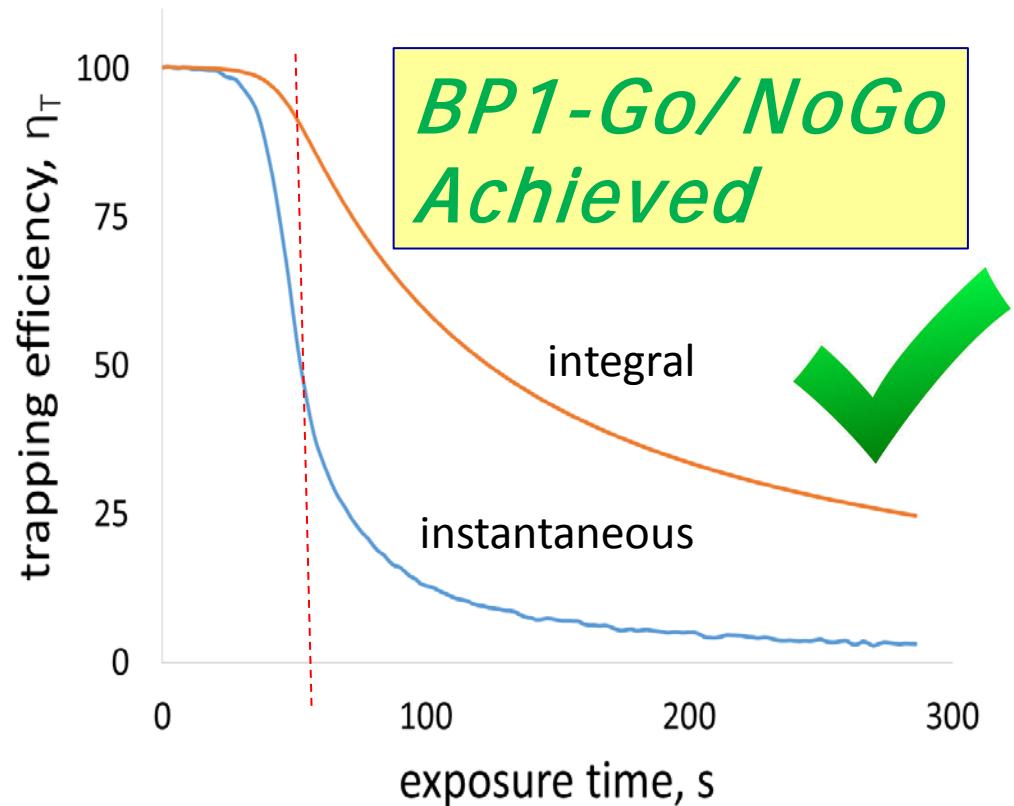
NOx trapping efficiency

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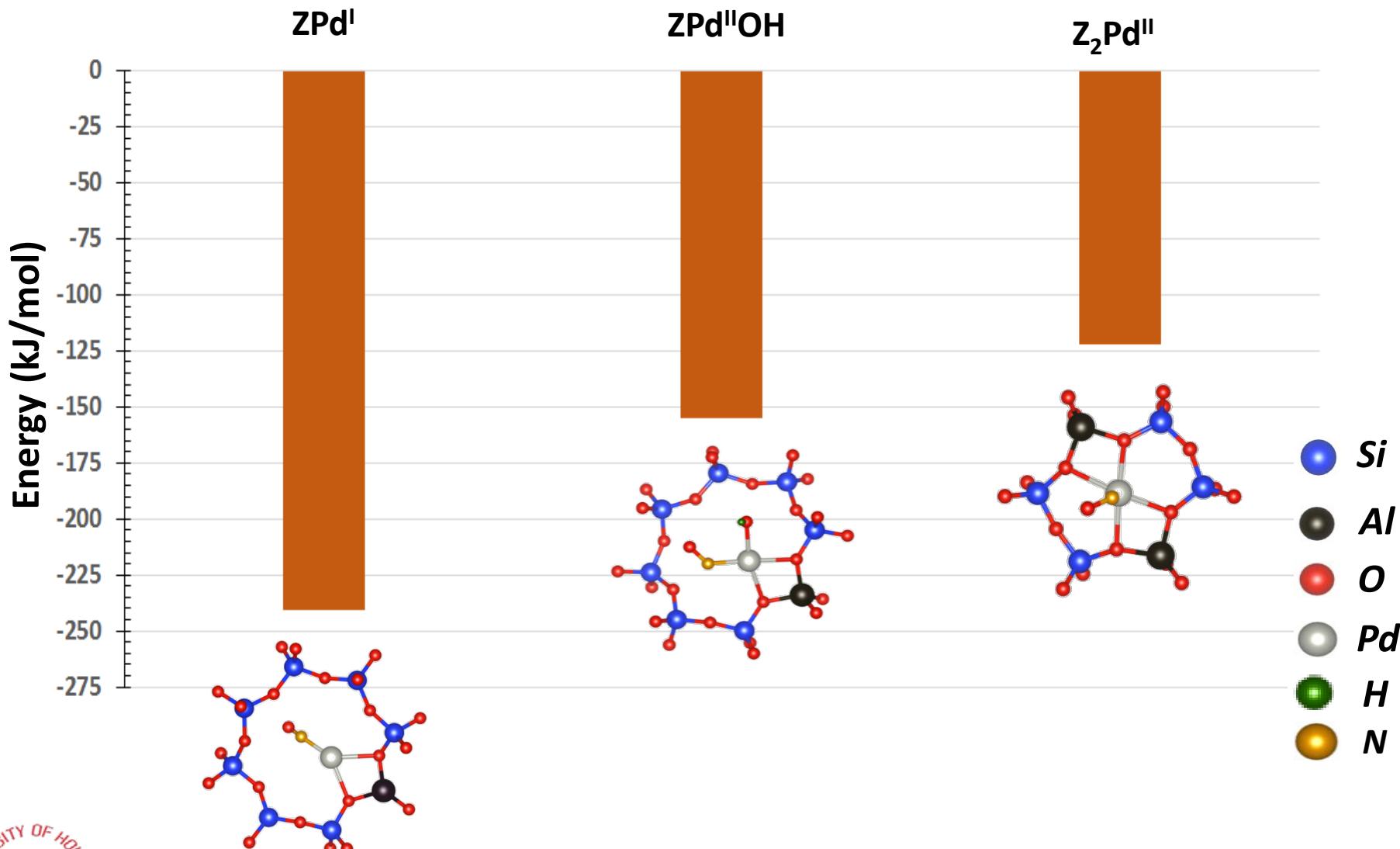
- Baseline PNA captures all of the NOx for ~ 1 minute for full USDRIVE feed mixture

NO/Pd ~

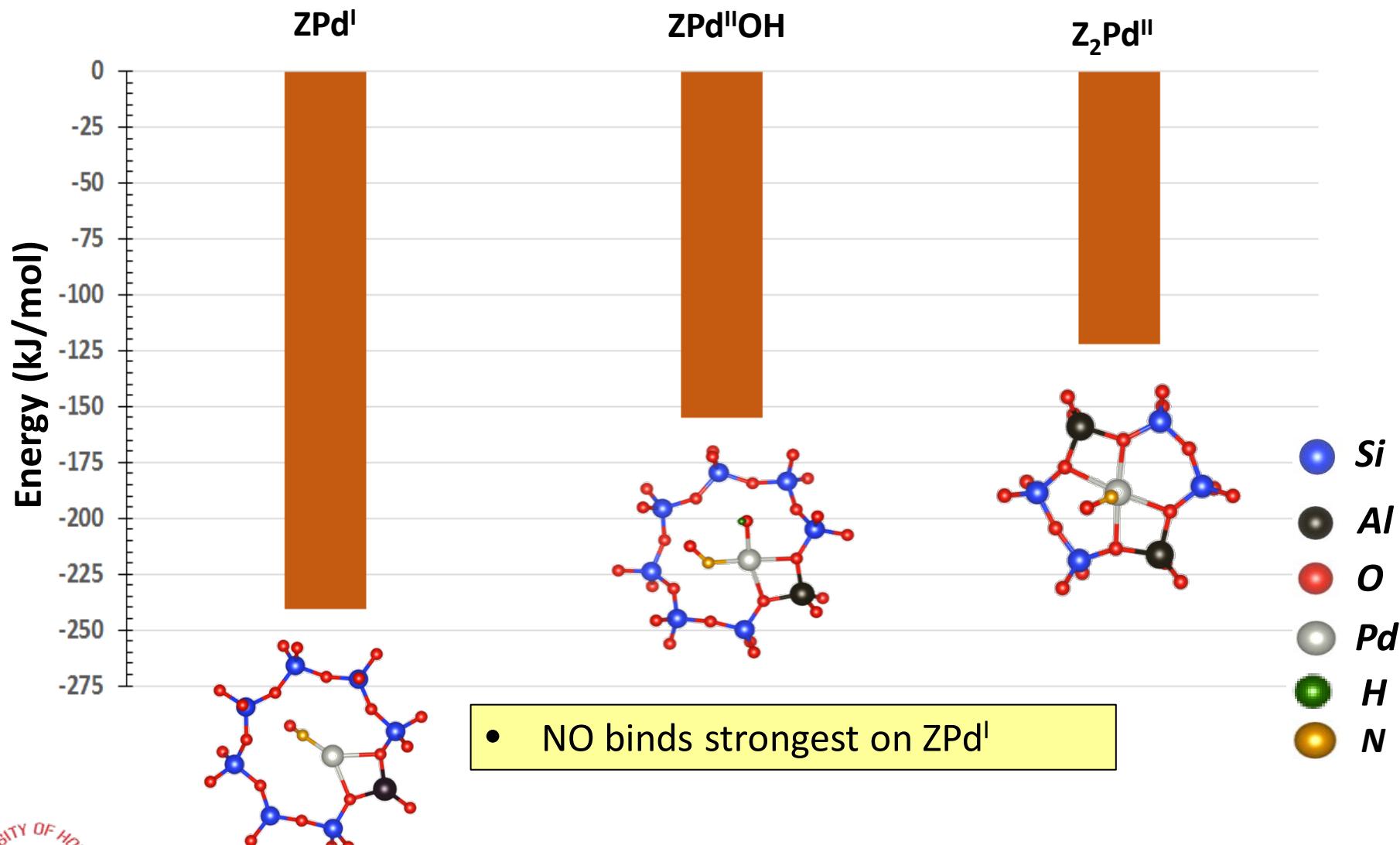
→ Efficient material for NOx trap and release



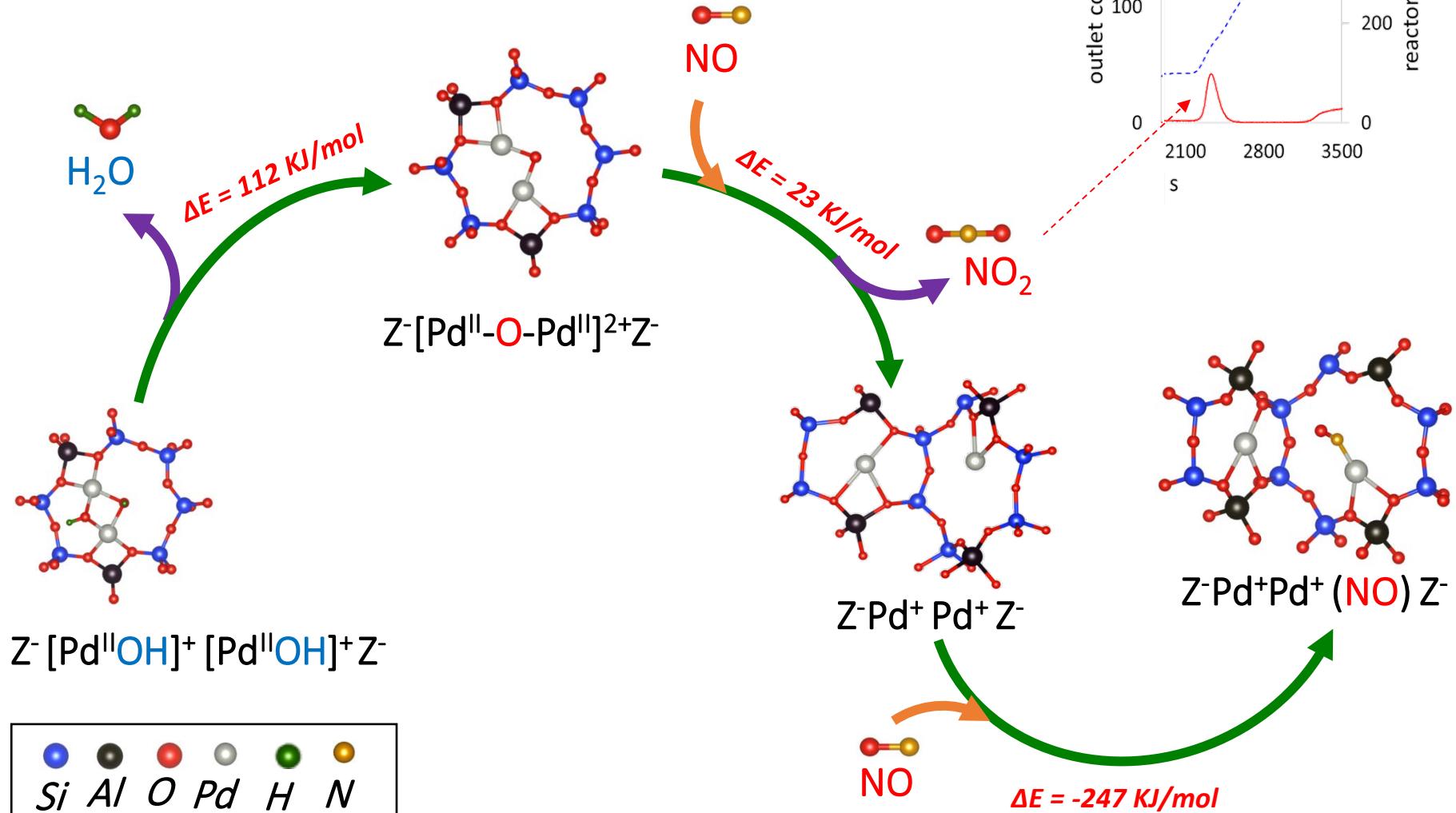
NO adsorption energy on Pd cation sites



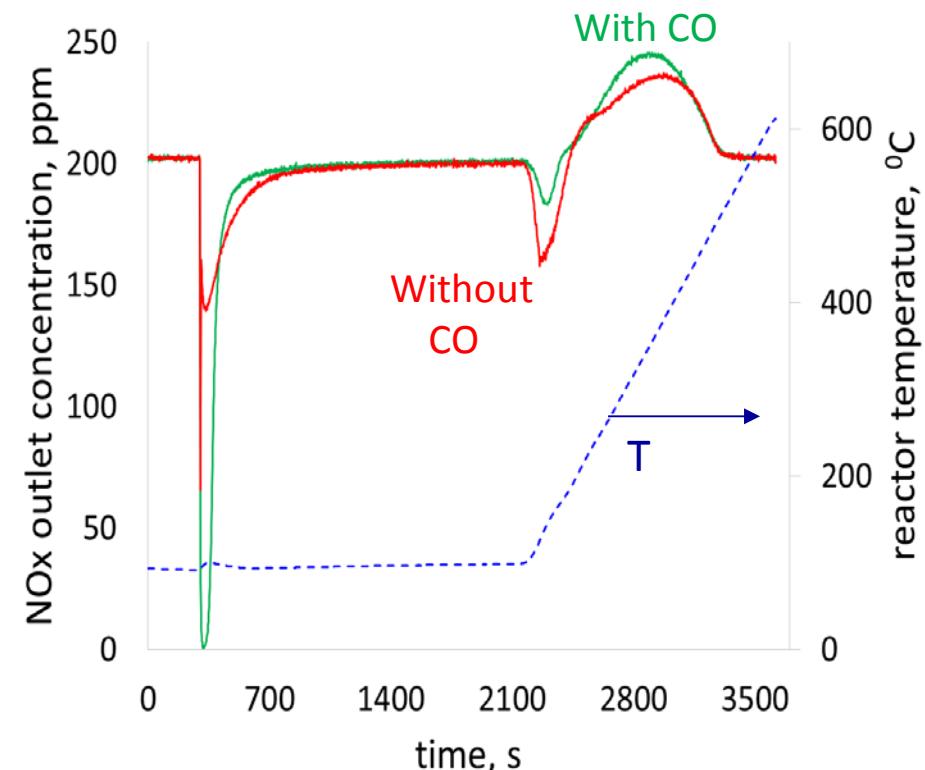
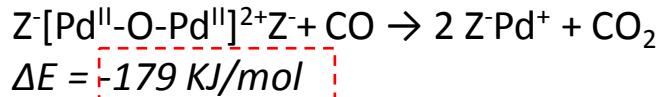
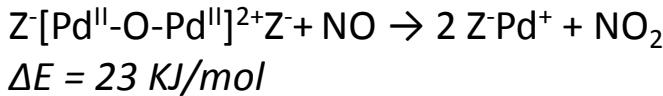
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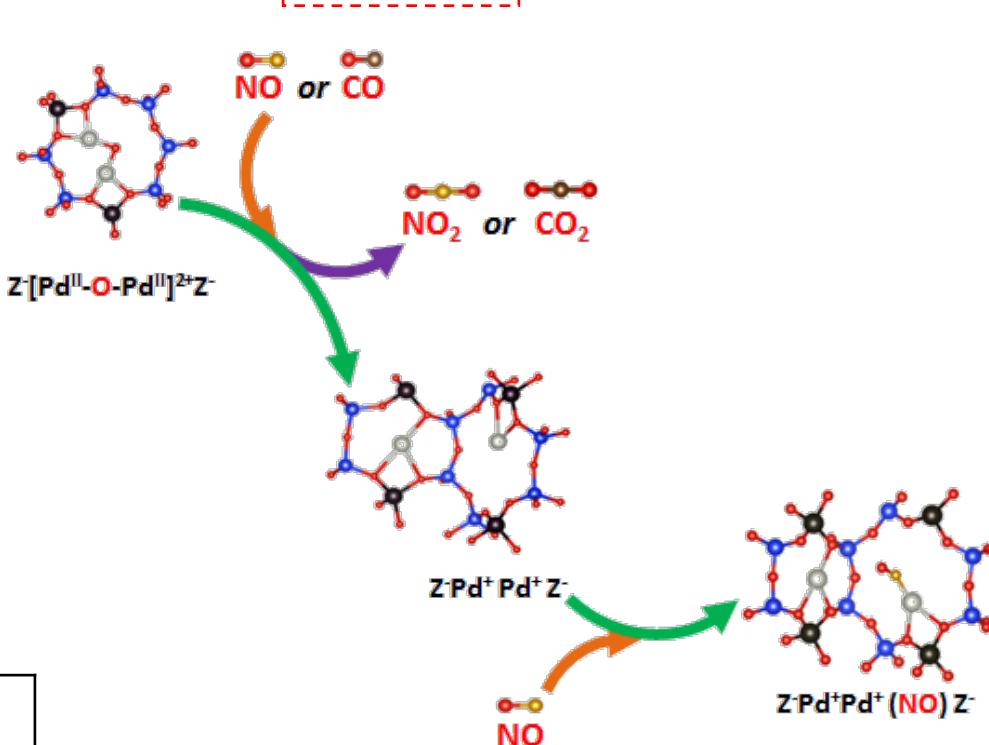
Formation of ZPd^I sites



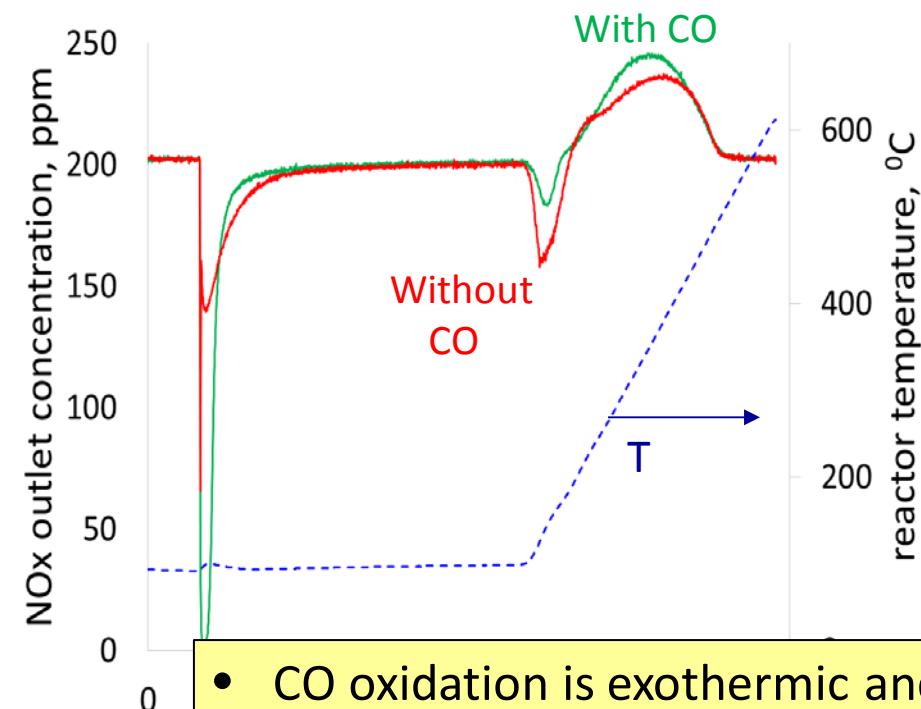
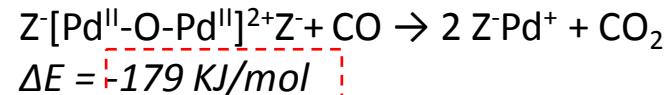
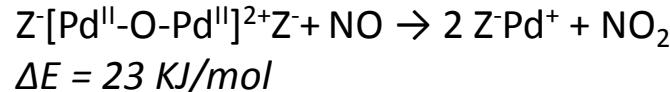
NO uptake and release in presence and absence of CO



NOx (ads)/NOx(des)	NOx/Pd
~ 1	~ 1.2

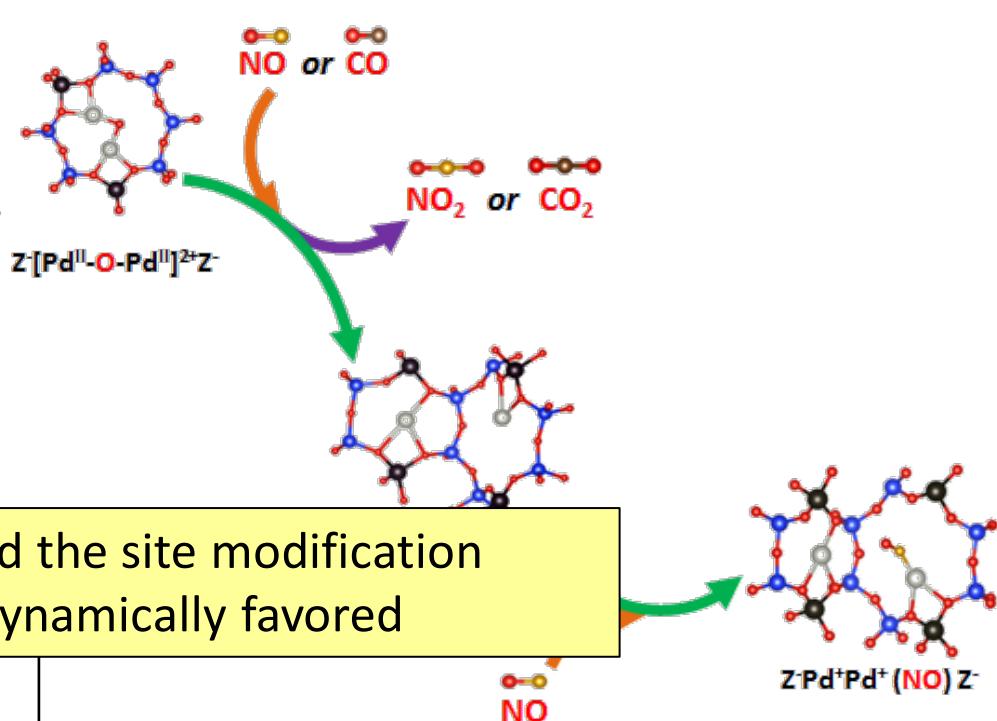


NO uptake and release in presence and absence of CO

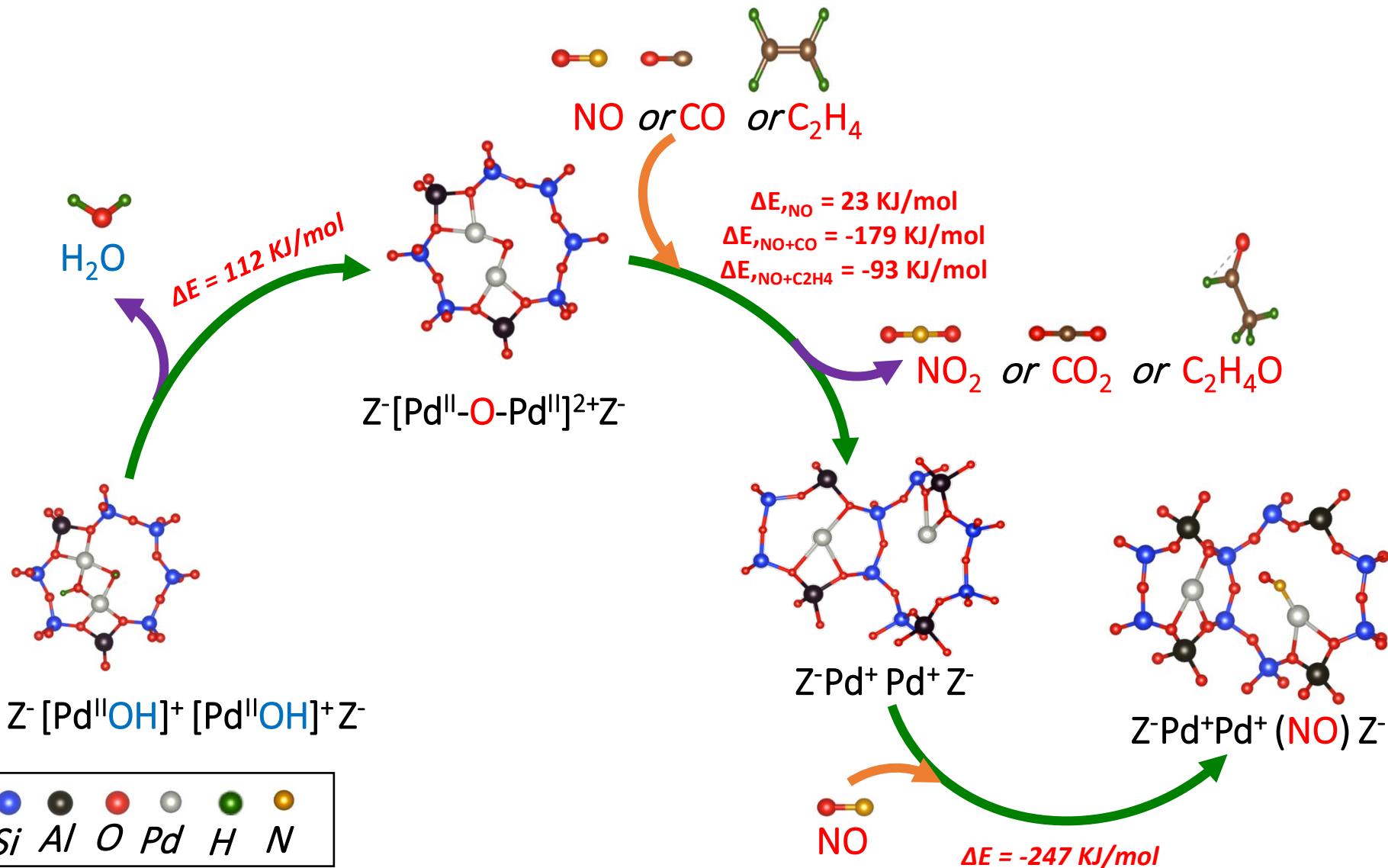


- CO oxidation is exothermic and the site modification from Pd^{II}OH to Pd⁺ is thermodynamically favored

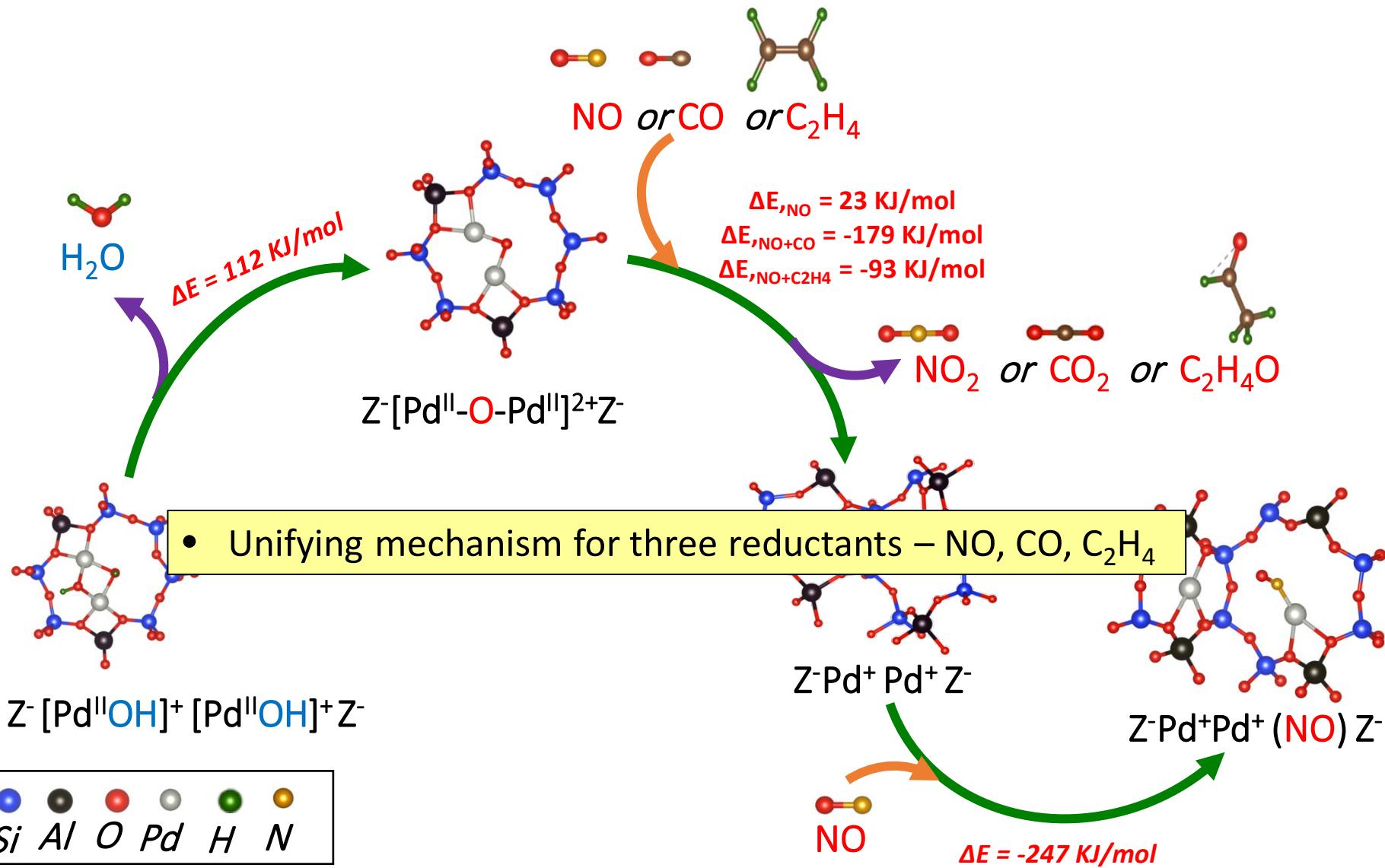
NO _x (ads)/NO _x (des)	NO _x /Pd
~ 1	~ 1.2



NO trapping mechanism in the presence of reductant

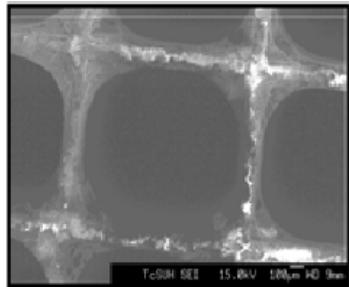
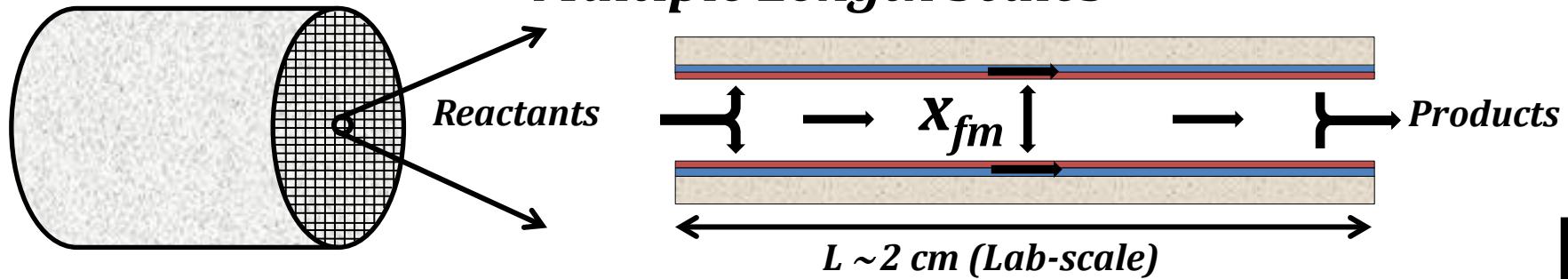


NO trapping mechanism in the presence of reductant

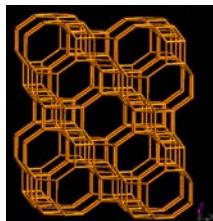


Monolith reactor model

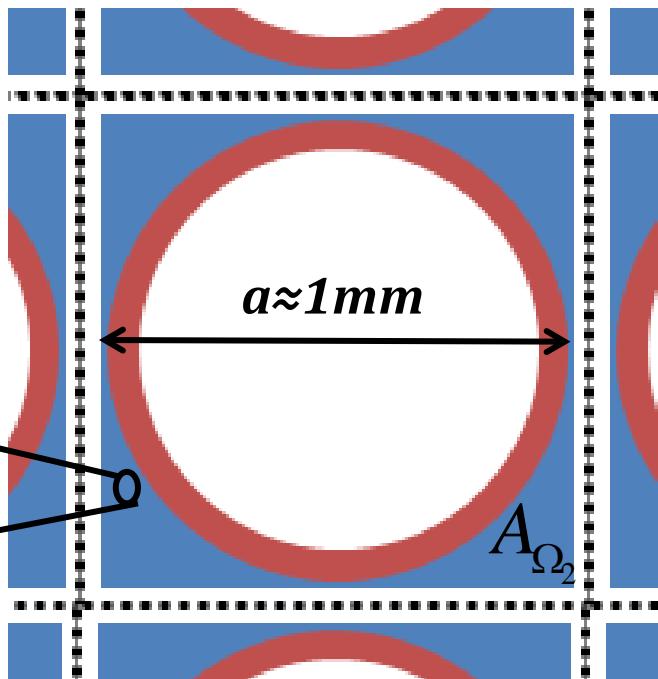
Multiple Length Scales



Zeolite Crystallites - 1- 3 μm



Pore Size
0.35 - 0.65 nm



Multi-layer Washcoat

$$R_{\Omega_2} = \frac{A_{\Omega_2}}{P_{\Omega_2}}$$

$\approx 10 - 50 \mu\text{m}$

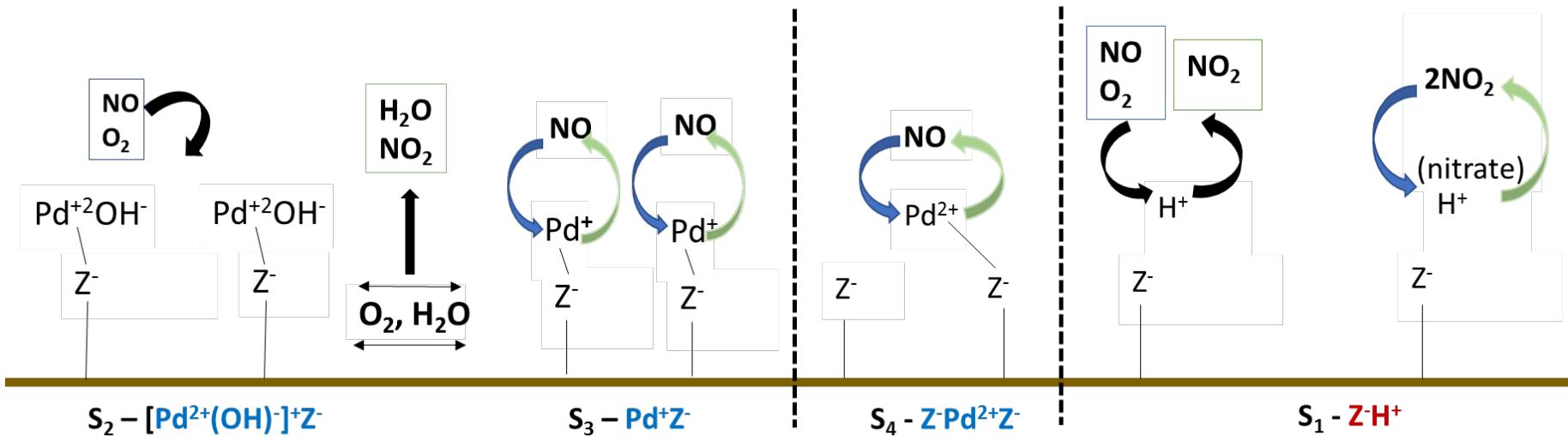
PNA microkinetic model (Pd/H-ZSM-5)

Scheme

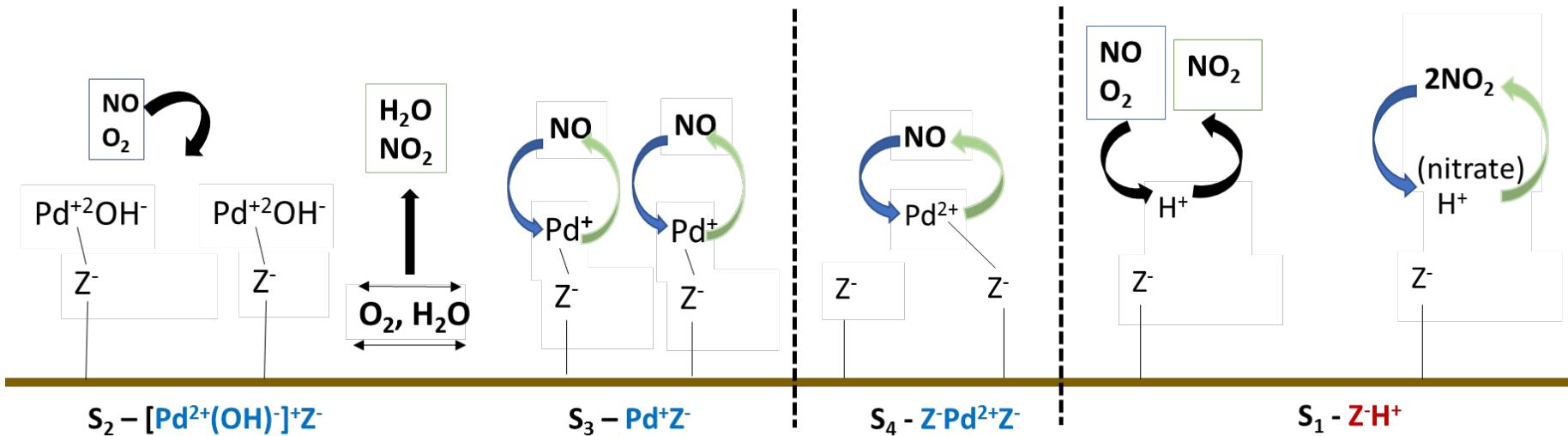
- Build mechanism using combination of literature, molecular modeling (DFT), & experiments [kinetics, flow reactor, DRIFTS, etc.]
- Use calculated energy barriers from DFT, when literature estimates not available
- Estimate remaining parameters from “fitting” uptake + release, in sequence:
 - NO + O₂ on H-ZSM-5
 - NO + O₂ + H₂O on **H-ZSM-5**
 - NO + O₂ on **Pd-H-ZSM-5**
 - NO + O₂ + H₂O on **Pd-H-ZSM-5**
 - NO + O₂ + H₂O + reductant (CO, C₂H₄, etc.) on **Pd-H-ZSM-5**
- Validate at other conditions, catalyst compositions, etc.
- Use model to define new experiments
- When satisfied, use model to optimize PNA material



PNA microkinetic model (Pd/H-ZSM-5)



PNA microkinetic model (Pd/H-ZSM-5)



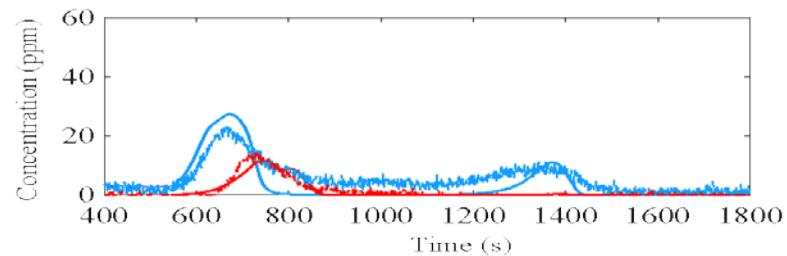
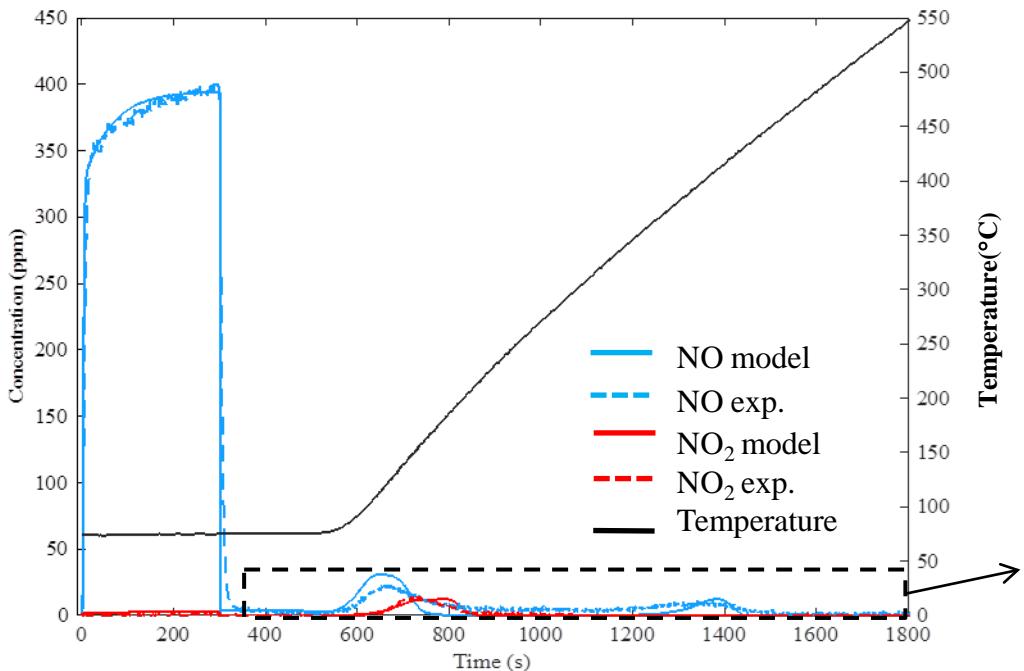
- Model accounts for key active sites confirmed from DFT calculations and DRIFTS measurements



PNA microkinetic model (Pd/H-ZSM-5)

NO + O₂ + H₂O on 2wt.% Pd-H-ZSM-5 (VALIDATION)

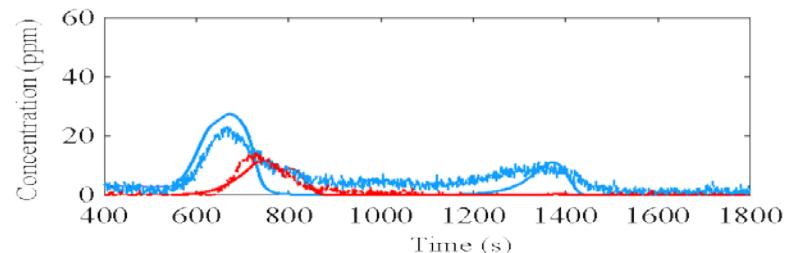
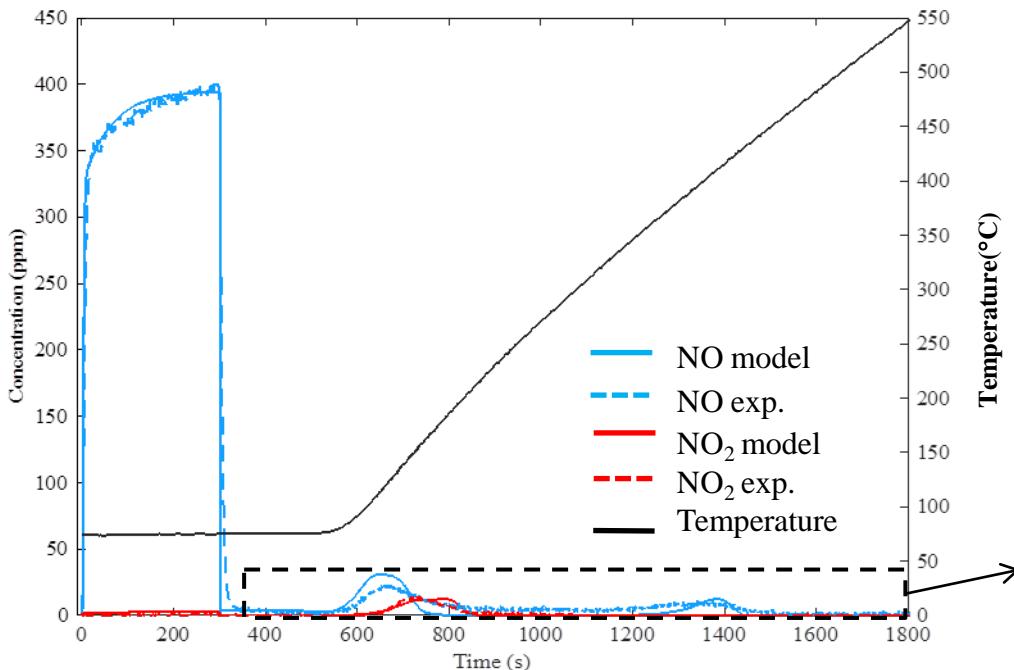
NO_x uptake at 80°C uptake & 1500 sccm



PNA microkinetic model (Pd/H-ZSM-5)

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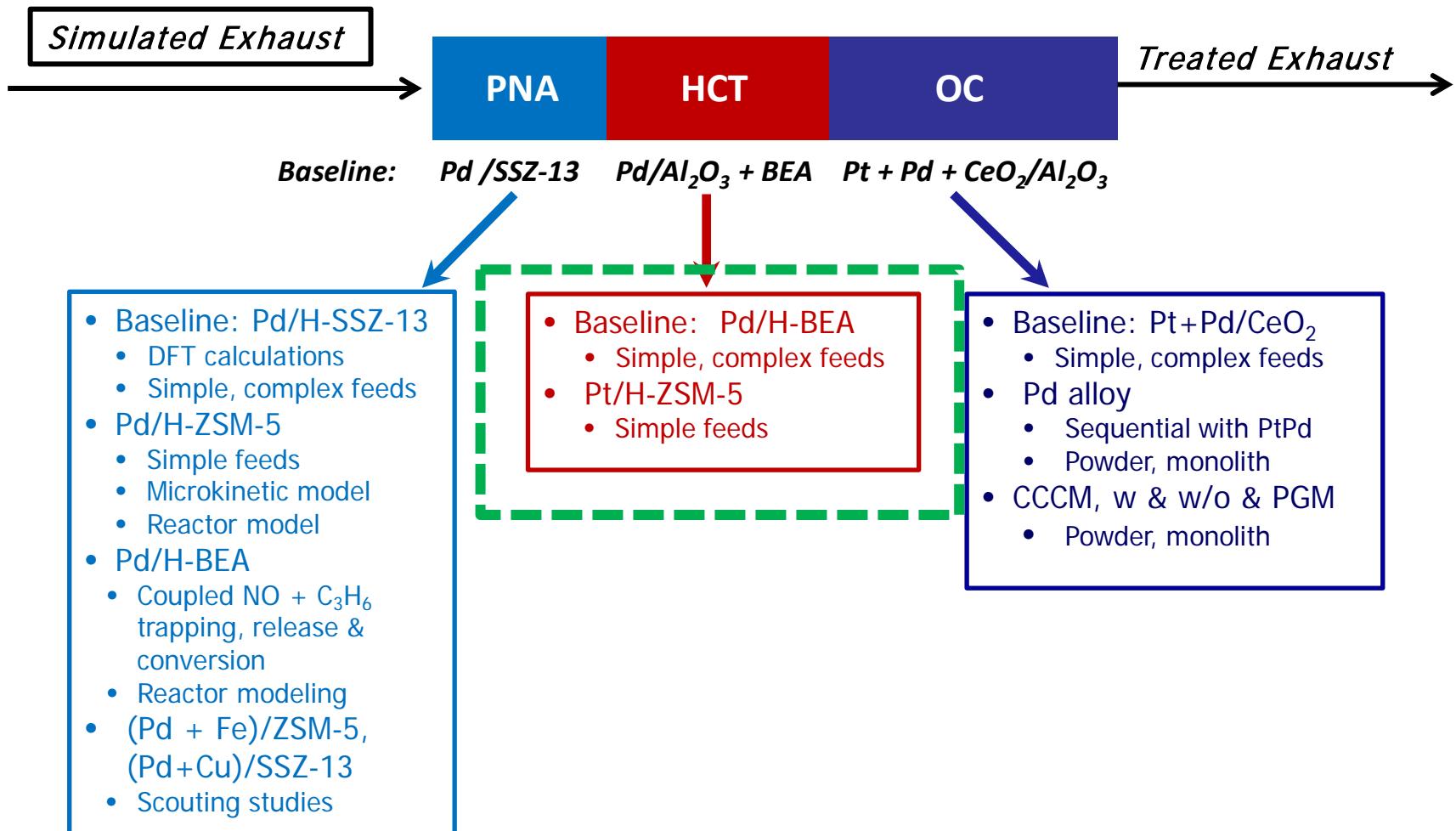
NO_x uptake at 80°C uptake & 1500 sccm



- Model validated at higher Pd loading



Project Activities



Hydrocarbon trap evaluations

- **Objective:** Evaluate uptake, release, and conversion of Clean Diesel (CD) feed on Baseline HCT (Pd/H-BEA) to quantify:
 - Uptake amount as function of time, temperature, etc.
 - Interaction effects between different feed components
 - Release and light-off temperature for different feeds
- **Status:**
 - Have evaluated for most binary mixtures and full feed; e.g.

Dodecane + Ethylene: 58 ppm dodecane, 200 ppm ethylene

Dodecane + CO: 58 ppm dodecane, 500 ppm CO

Dodecane + NO: 58 ppm dodecane, 200 ppm NO

Ethylene: 200 ppm ethylene

Ethylene + NO: 200 ppm C₂H₄, 200 ppm NO

Ethylene + CO: 200 ppm C₂H₄, 500 ppm CO

etc.

CD Feed:

Species	Conc. (ppm)
NO	200
CO	500
H ₂	100
C ₂ H ₄	200
C ₇ H ₈	43
C ₁₂ H ₂₆	58

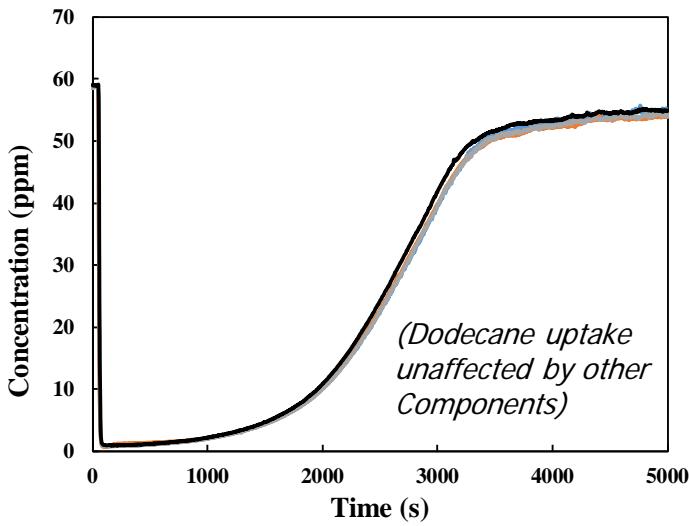
12% O₂,
6% CO₂,
6% H₂O,
Balance N₂



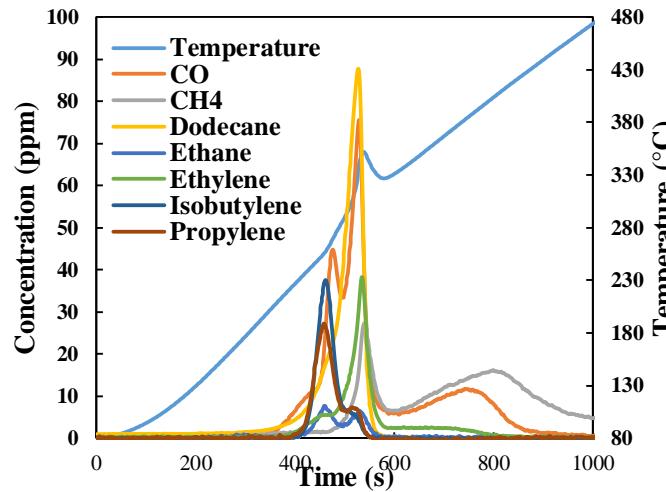
Hydrocarbon trap evaluations

Feeds: Dodecane & Dodecane + CO

Dodecane Uptake



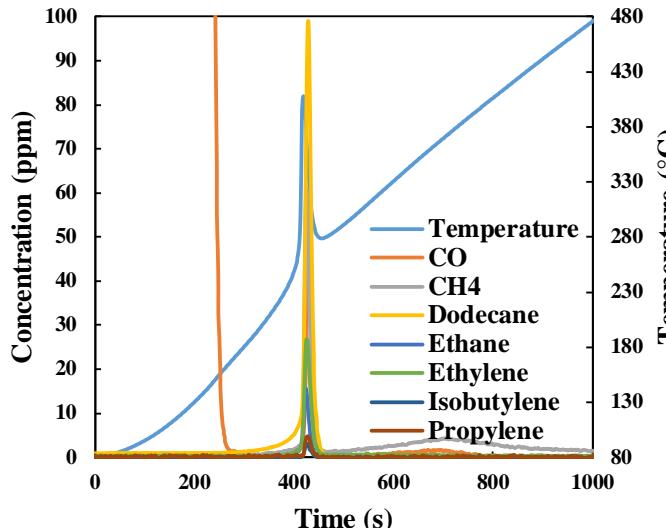
TPD – Dodecane



Feeds:

Species	Conc. (ppm)
CO	500
$C_{12}H_{26}$	58

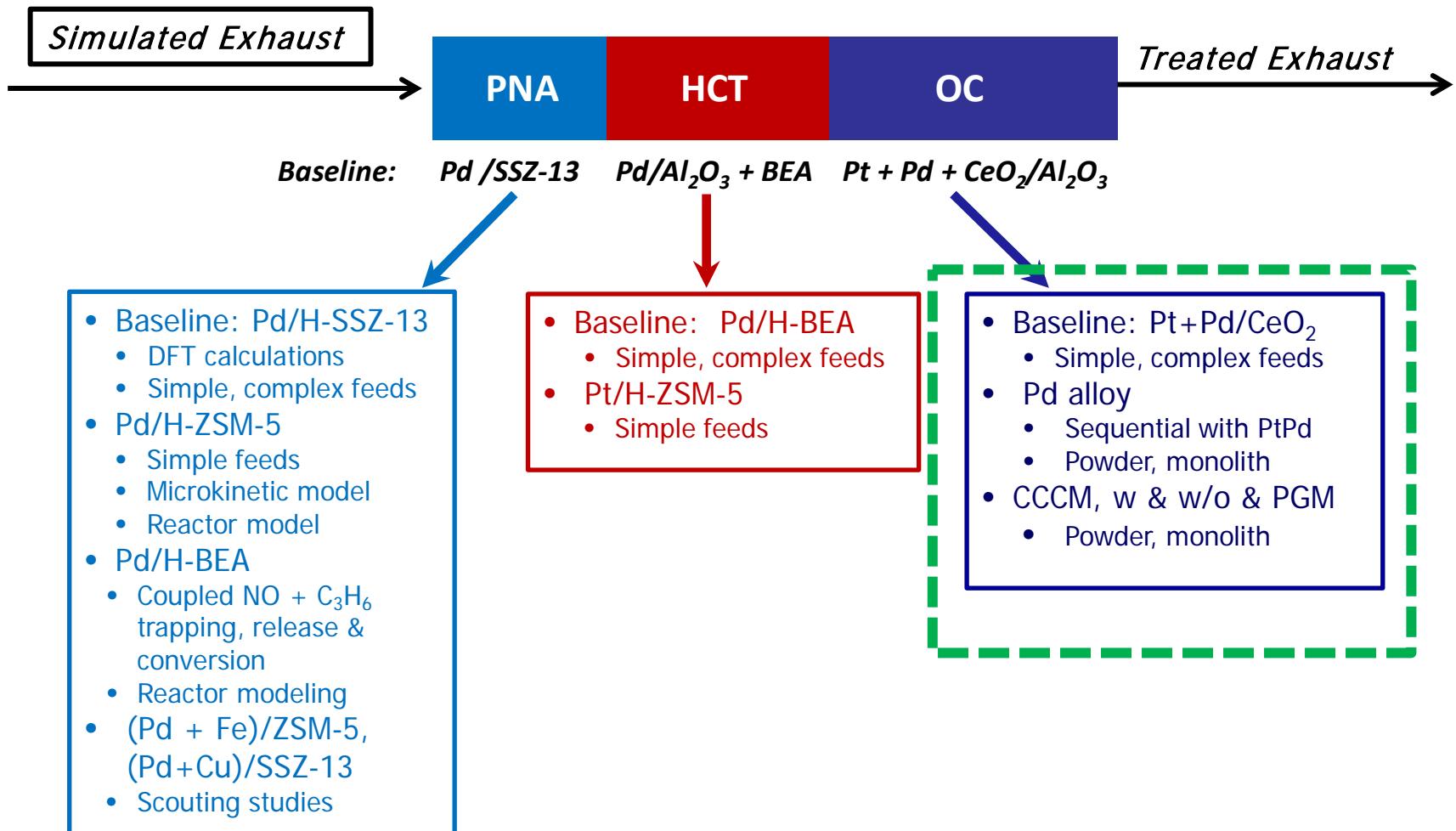
TPD – Dodecane + CO



12% O_2 ,
6% CO_2 ,
6% H_2O ,
Balance N_2



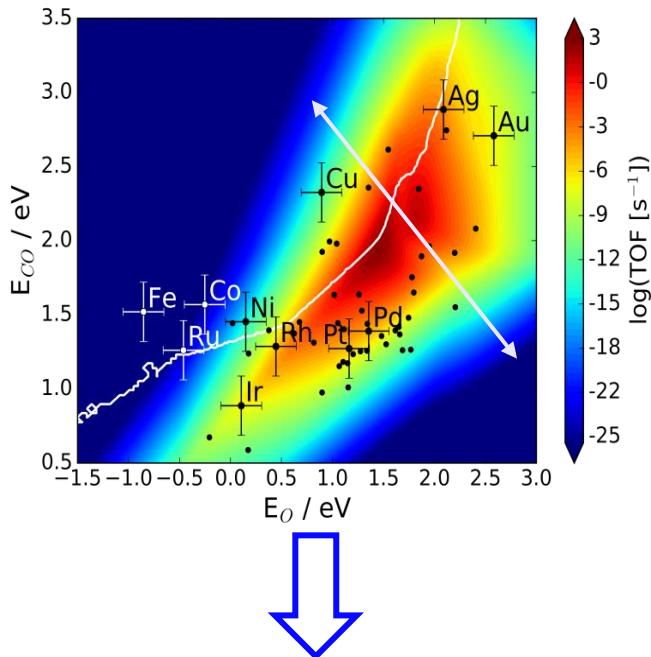
Project Activities



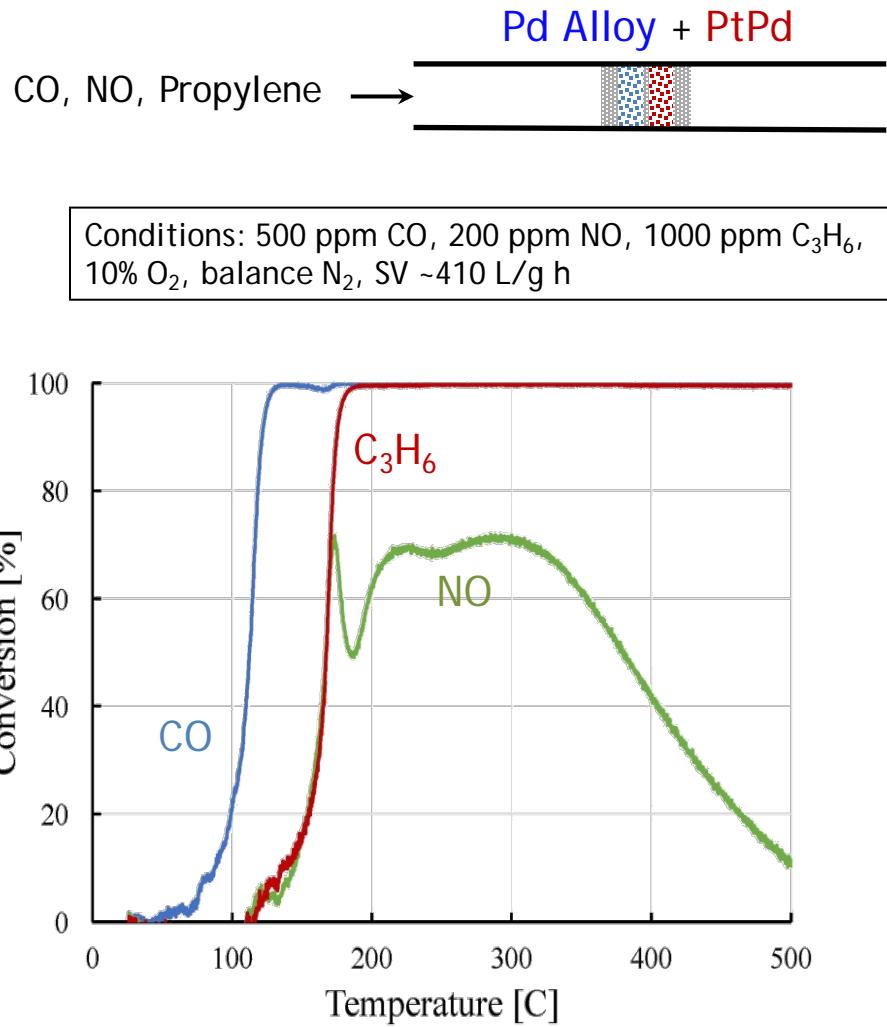
Low temperature oxidation catalyst for low co-oxidation of NO, CO & C₃H₆

UNIVERSITY OF HOUSTON
COLLEGE OF ENGINEERING

Descriptor DFT



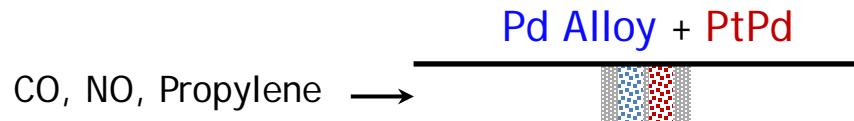
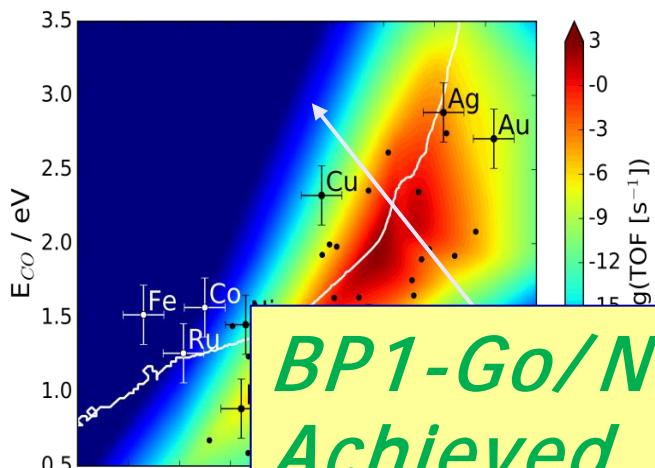
Promising Pd alloy: High CO + NO co-oxidation activity with resistance to mutual inhibition



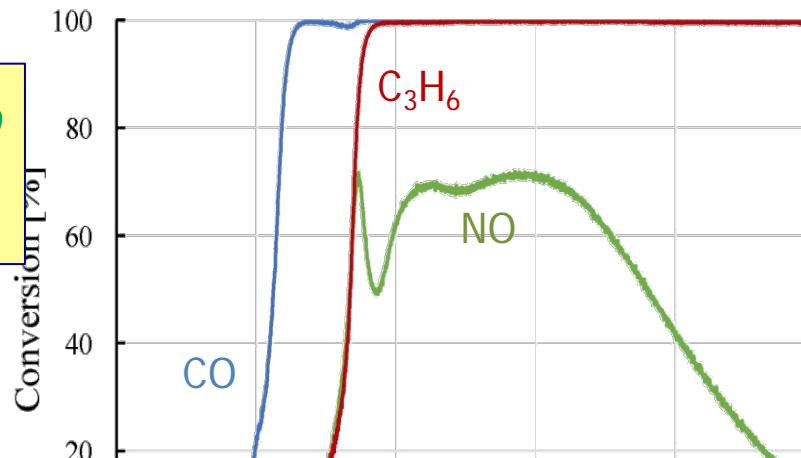
Low temperature oxidation catalyst for low co-oxidation of NO, CO & C₃H₆

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Descriptor DFT



Conditions: 500 ppm CO, 200 ppm NO, 1000 ppm C₃H₆, 10% O₂, balance N₂, SV ~410 L/g h

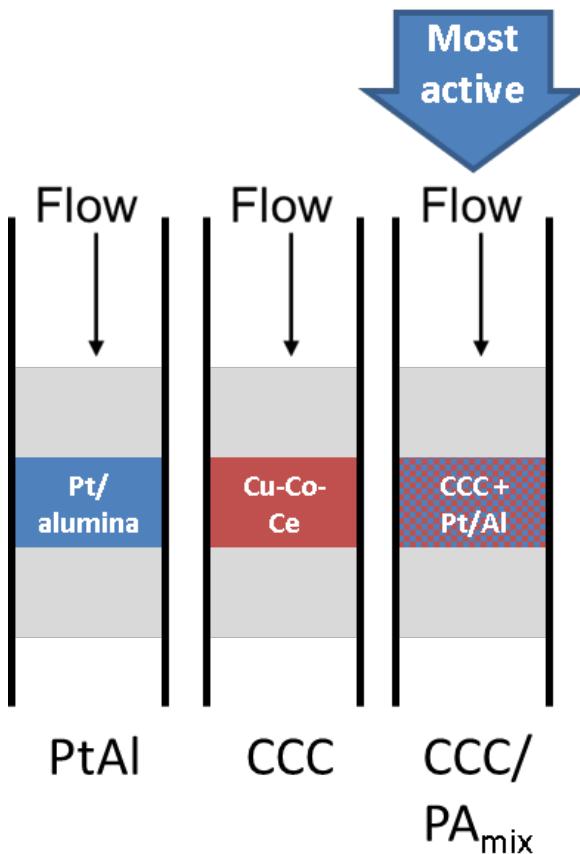


Promising Pd alloy: High CO + NO co-oxidation resistance

- Encouraging results for CO oxidation
- NO and HC oxidation below 150 °C remains a challenge



Low temperature oxidation catalyst: Co-oxidation of NO, CO & HCs



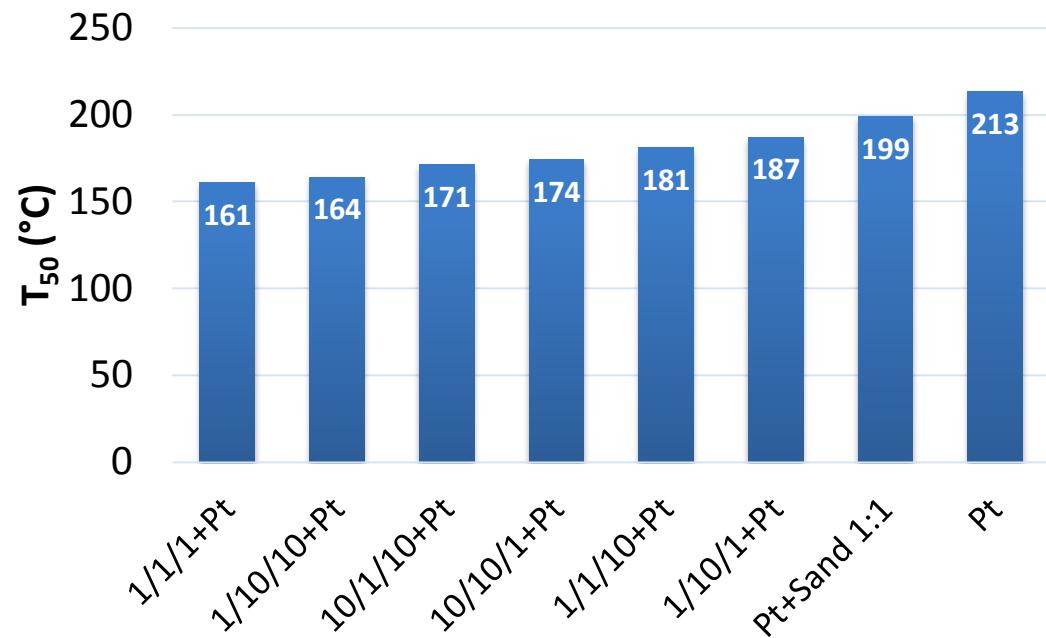
T₅₀ of THC Conversion

CCC + 1% Pt/Al₂O₃ (1:1 wt.)

[CO]: 10,000ppm

[C₃H₆]: 500ppm

[C₃H₈]: 500 ppm SV: 200 L/g h



CCC : Cu/Co/Ce mixed oxides with corresponding mass ratios #/#/#



Remaining Challenges & Barriers

- Good progress on BP1 & BP2 tasks and milestones
- Further development of new PNA, HCT, and OC materials
- Overcome mutual inhibition of NO and HC trapping
- Demonstrate consolidation of trapping & catalytic functions



Proposed Future Work

- Focus: BP2 milestones
- Continue descriptor DFT to identify new PNA, HCT, OC
- Target: Pd + M/H-SSZ-13 (PNA), CCC + Pt (OC)
- Use TAP + DRIFTS for mechanistic-based understanding and microkinetic model development
- Extend microkinetic + reactor model to Pd/H-SSZ-13
- Combine PNA + HCT + OC functions in sequence & parallel, including Pd/BEA + Pd/SSZ-13
- Expand reactor model for combined system



BP2 Milestones

BP2-M#	Milestone	Type	Description	Status
BP2-M1	Additional materials discovery completed	Technical	Identify at least three additional materials from descriptor-based DFT.	Identified new PNA materials; Pd+Cu/SSZ-13, Pd+Fe/SSZ-13
BP2-M2	Microkinetic model development validated	Technical	Develop, tune and validate microkinetic models for new LHCNT materials for HC trapping, HC oxidation, and NO adsorption.	Completed for PNA: Pd/ZSM-5 & underway for Pd/SSZ-13; Underway for HCT: Pd/BEA and HC oxidation
BP2-M3	New material performance testing completed	Technical	Complete flow reactor performance testing of LHCNT material containing one or more new functions for HC trapping, HC oxidation, and NO adsorption, and compare performance to baseline LHCNT material.	Underway for sequential PNA + OC, dual-layer PNA+HCT+OC, and sequential CCC + PGM
BP2-M4	Monolith reactor model comparison of baseline and new materials	Technical	Develop, tune and validate monolith reactor model of new LHCNT material and compare to baseline LHCNT material.	Kinetic/reactor model complete for NO trapping on Pd/ZSM-5; underway for Pd/SSZ-13 and Pd/BEA
BP2-Go/NoGo	Identification of candidate material	Go/No Go	Develop and demonstrate predictive model that predicts performance of baseline LHCNT and which can be used for optimization.	Model for PNA with NO + CO + HC feed to be used to optimize material;.



Summary

■ Relevance

- Enabling emergence of advanced, low temperature combustion engines

■ Approach

- Development of integrated NO + HC catalytic trap
- From molecular-level discovery & mechanism to development & demonstration

■ Technical Accomplishments & Progress

- Good progress on all fronts; BP1 milestones achieved
- PNA results encouraging; leads on new OC materials
- PNA + HCT + OC baseline materials demonstrated

■ Collaborations & Coordination

- Cooperation: universities (UH+UVA), labs (ORNL+SwRI), industry (JM+FCA)

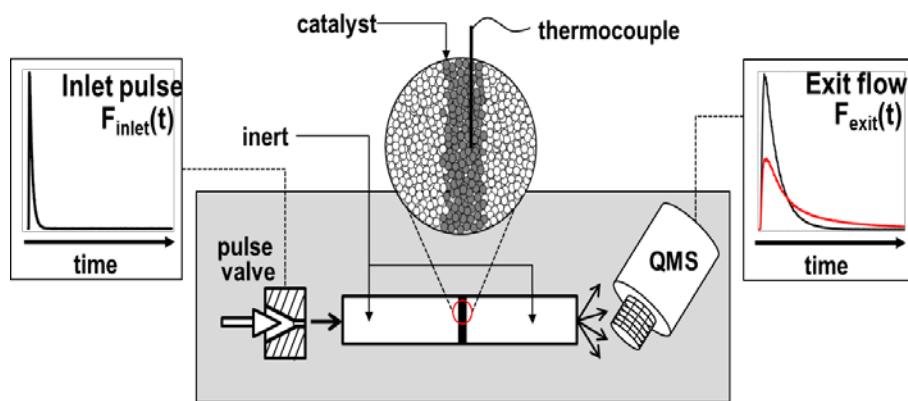
■ Proposed Future Research

- Convergence of materials, refinement, integration, modeling, & optimization

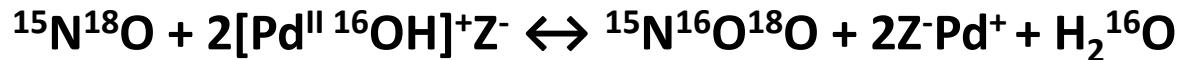
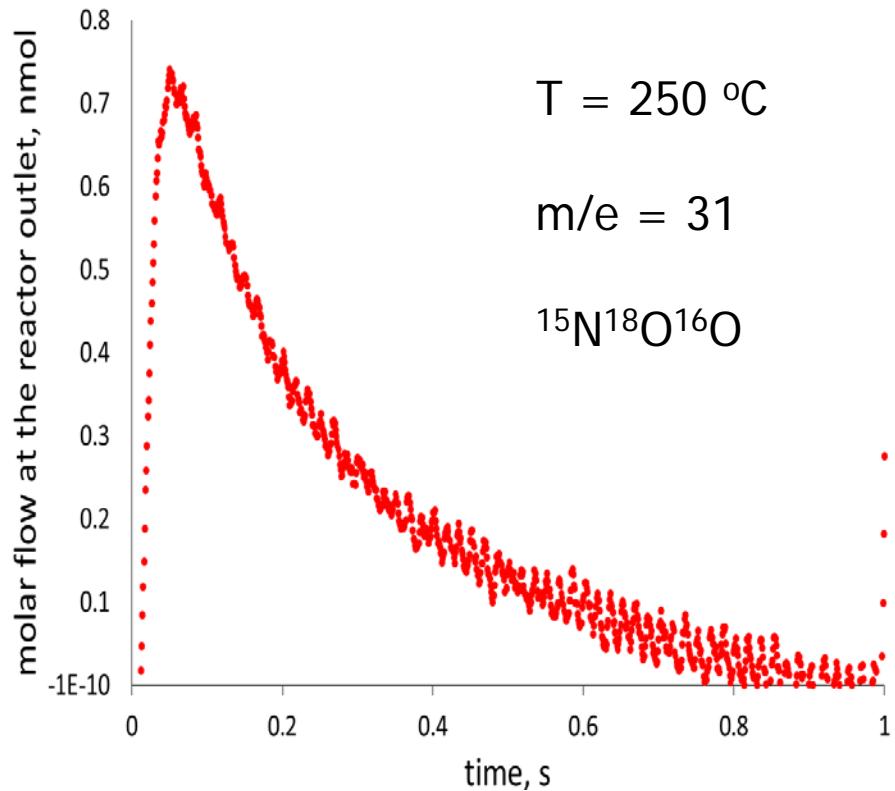


Technical Backup Slides

Isotopic labeling studies in TAP reactor



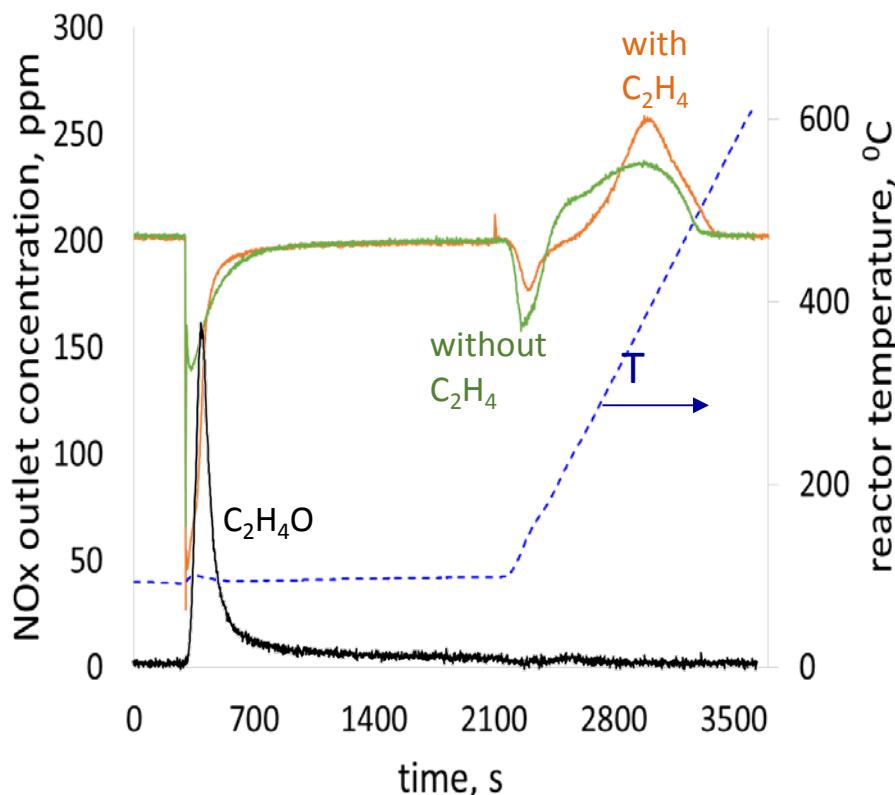
Catalyst pretreated with $^{16}\text{O}_2$ and pulsed with $^{15}\text{N}^{18}\text{O}$



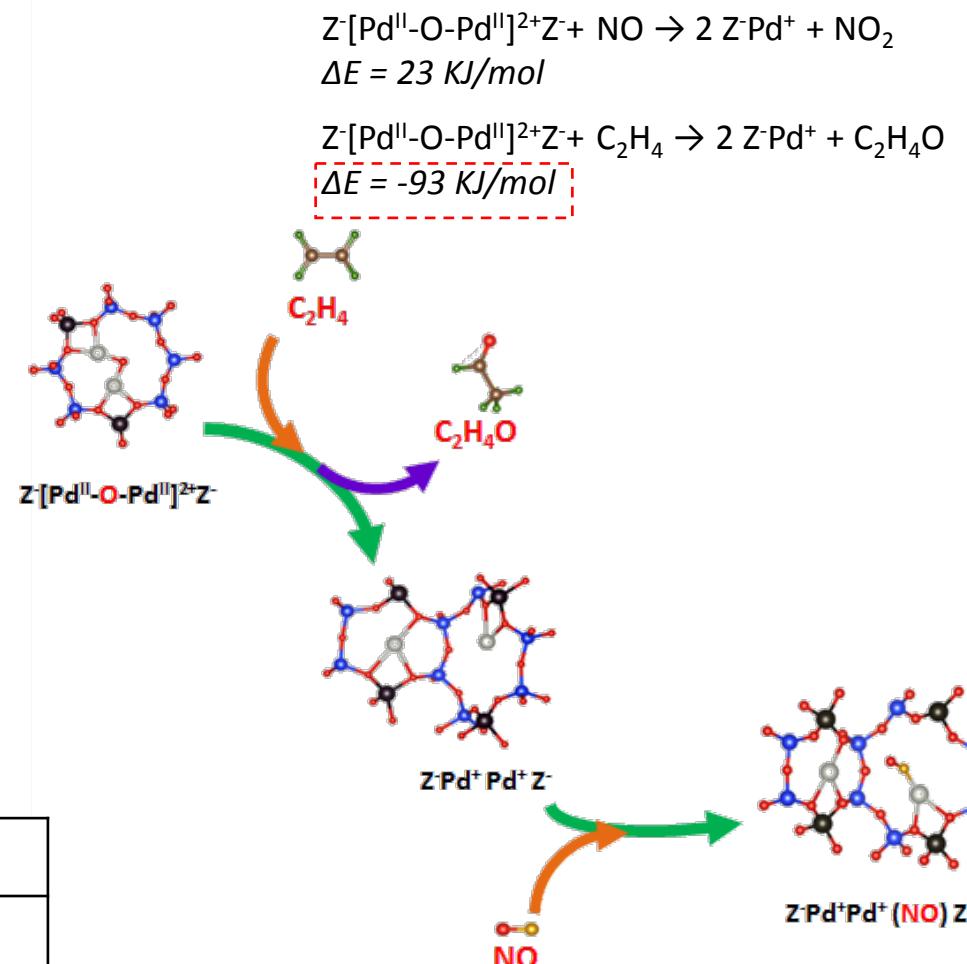
- Isotopic exchange of oxygen is consistent with DFT postulated reduction step



NO uptake and release in the presence of ethylene

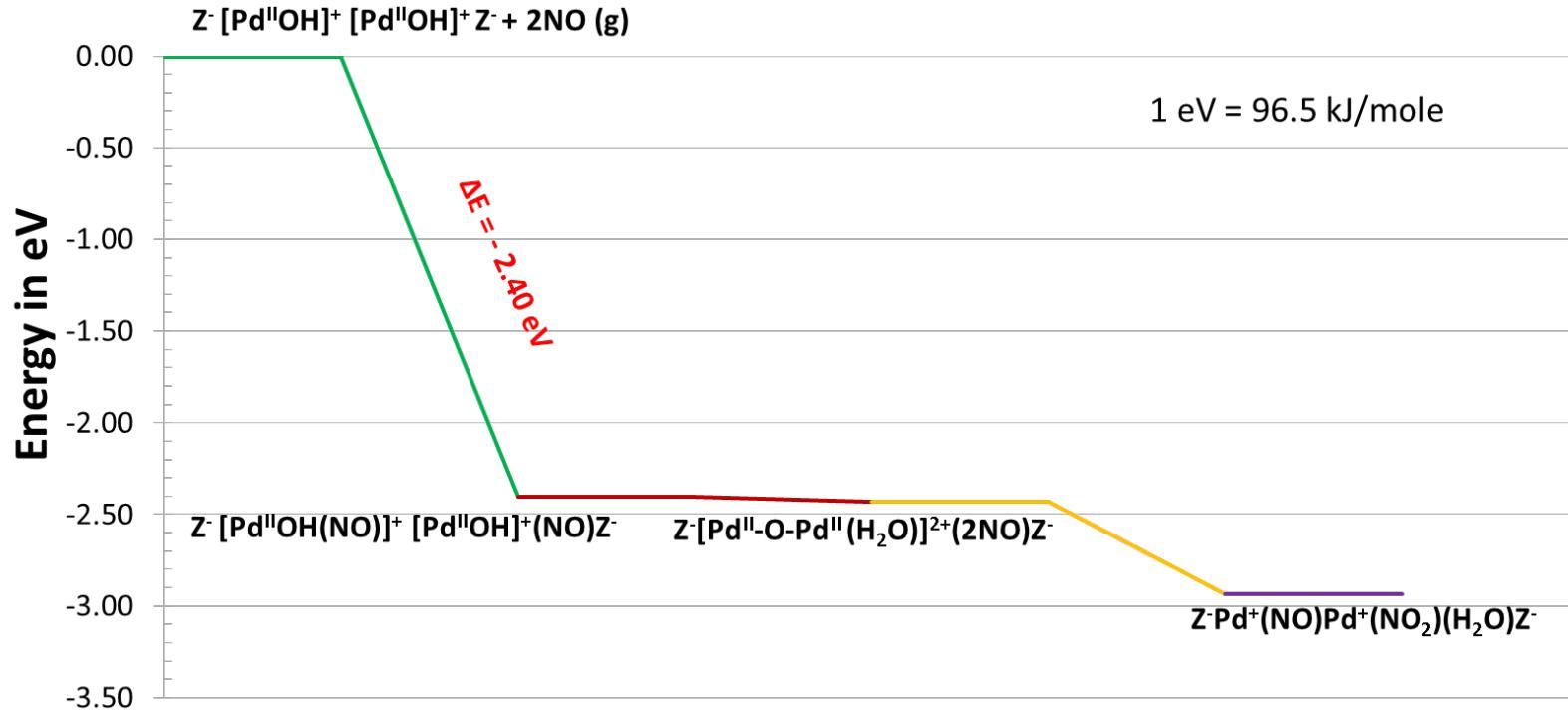


NOx (ads)/NOx(des)	NOx/Pd
~ 1	~ 1.2



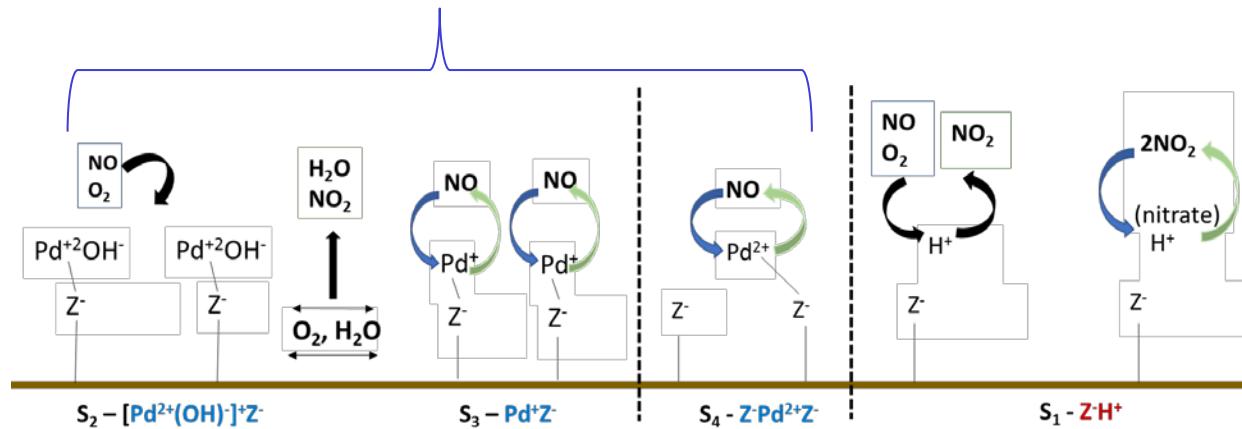
C_2H_4 oxidation is more exothermic and the site modification from $\text{Pd}^{\text{II}}\text{OH}$ to Pd^+ is thermodynamically favored with C_2H_4

Alternative NO uptake pathway forming NO-Pd(I)



PNA microkinetic model (Pd/H-ZSM-5)

Pd-ZSM-5



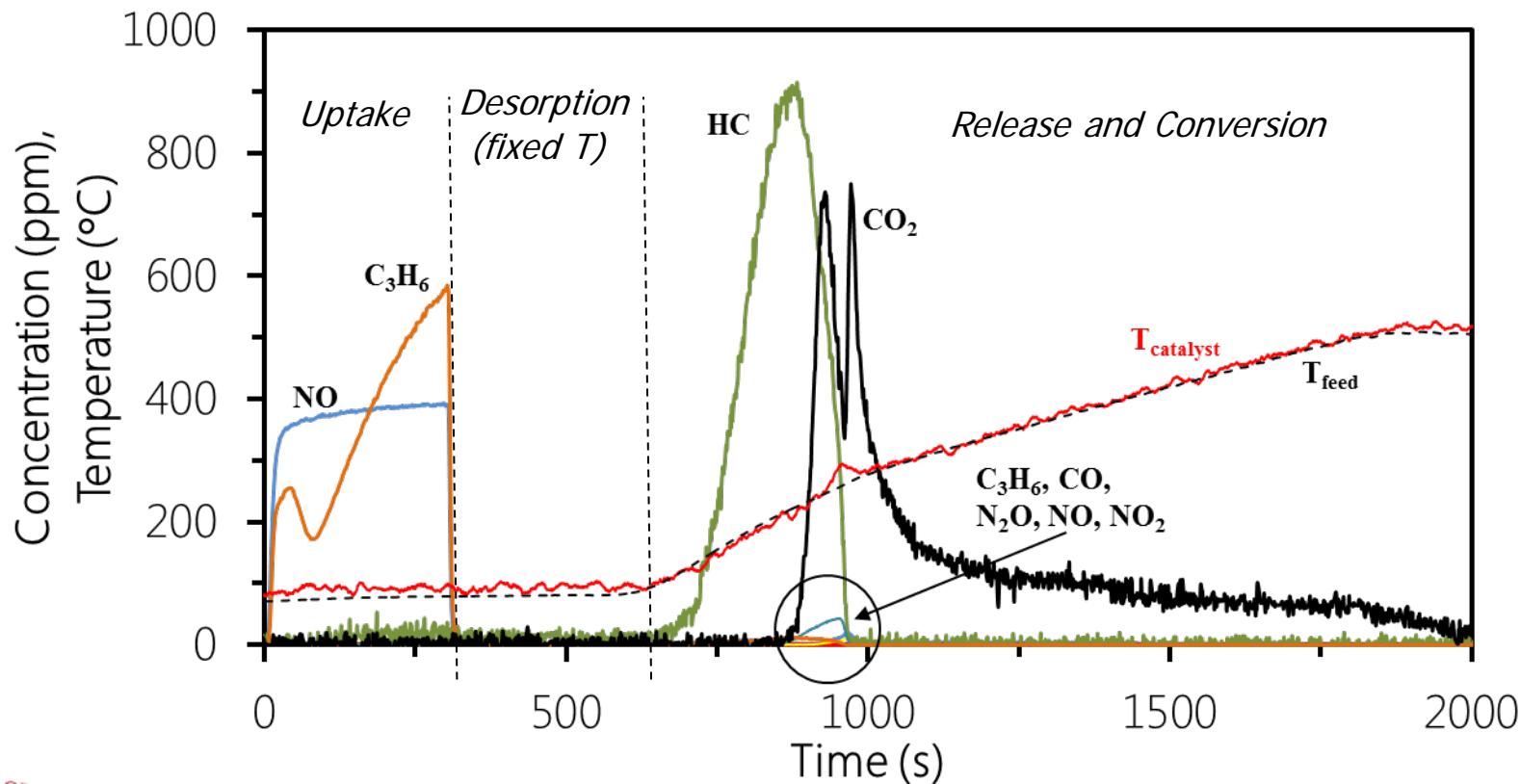
Coupled NO + HC Trapping, Release & Conversion: Pd/H-BEA

Uptake Temperature: 80°C

Feed: 400 ppm NO, 800 ppm C₃H₆, 2% O₂

2wt% Pd-BEA, Si/Al = 19

1.5g wc/in³; Al/Pd= 3.4



- Trap NO + HC at low temperature, then releases and oxidizes during temperature ramp